

Vibration measurements and strategics in analyzing pipe vibration and pipe support damages

A consideration of pipe vibration measurements due to good and bad experiences

Disposition

- Why pipe vibration measurements?
 - Standards
 - Damages
- What are we facing
- Recommendations

Examples of evaluation criterias

ANSI/ASME OM3-1982, procedure 1

$$V_{allow} = \frac{C_1 \cdot C_2 \cdot (0.8 \cdot S_u) \cdot 3.64 \cdot 10^5}{C_3 \cdot C_4 \cdot K_2}$$

C_1 Factor for mass distribution
 C_2, K_2 Parameter for stress condition
 C_3 Factor for pipe contents and insulation
 C_4 Factor for restraints
 $(0.8 S_u)$ Fatigue limit

Seligman & Guillou

OK < 12 mm/s RMS @ PWR feedwater lines

Russian PTM 38.001-94

- I) No danger,
- II) Danger not probable
- III) Improvement is req. and damage is possible

	Frequency Hz									
	2	4	6	8	10	20	30	40	50	60
Area	Vibration Velocity in um									
I	250	230	200	180	165	120	95	85	75	70
II	500	450	400	360	330	230	190	145	135	130
III	1250	1100	950	800	750	500	420	350	320	300

Gamble & Tagart

OK < 0.5 mm for $f < 10$ Hz
 OK < 0.25 mm for $f < 10-40$ Hz
 Based on findings for
 400 pipe systems

Note: Indicated vib
 with good eng
 tions, unrein

VDI 2063

The requirements below
 should be fulfilled for
 2-300 Hz
 OK < 68 mm/s peak
 OK < 1 mm peak
 OK < 4 g peak
 + VDI 3842: Vibration in
 piping systems ?

Lloyds

OK < 35 mm/s peak
 Danger ≥ 70 mm/s peak

ABB

OK < 8 mm/s RMS
 Danger ≥ 20 mm/s RMS

Bild 2: Grenzkurve für harmonische (sinusförmige) Schwingungen. Für harmonische Schwingungsmischungen gelten die Bedingungen (7).

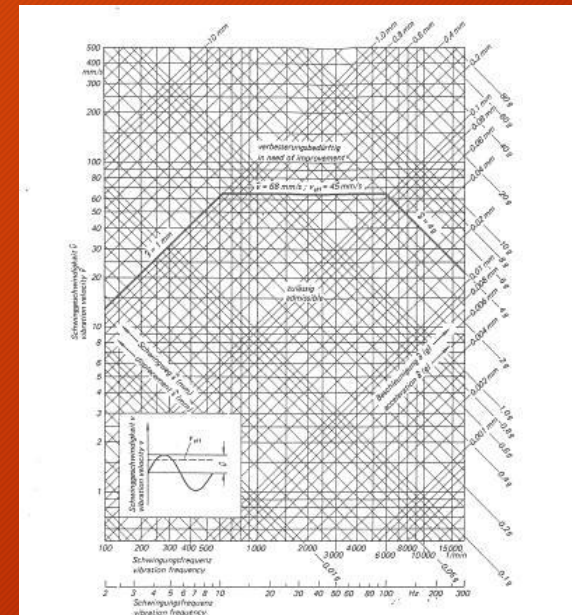


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Fig. 2: Limiting curve for sinusoidal vibrations. For composite vibrations the conditions (7) are valid.

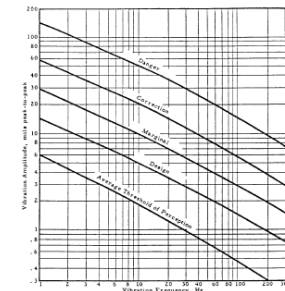


Figure 1. Allowable Piping Vibration Levels

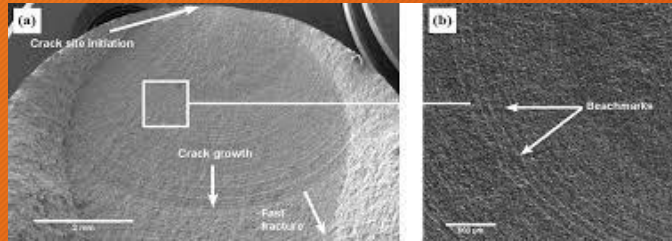
Note: Indicated vibration limits are for average piping system constructed in accordance with good engineering practices. Make additional allowances for critical applications, unreinforced branch connections, etc.

Wachel

Uninsulated pipe <
 304 mm/s peak
 Pipe with concentrated
 mass load <
 13 mm/s peak

2021-11-04

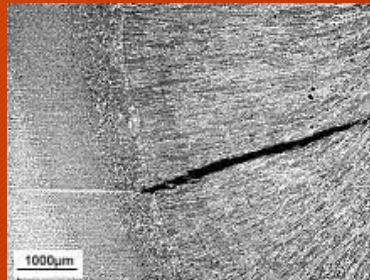
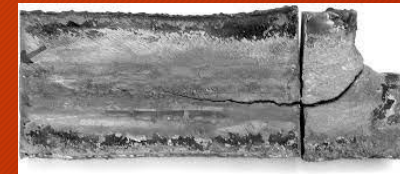
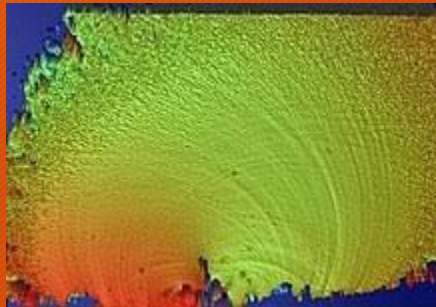
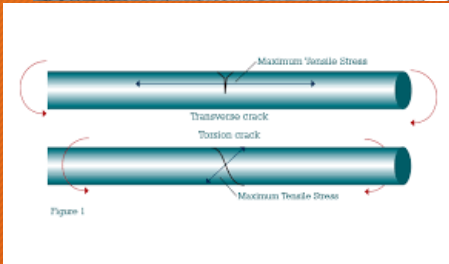
What type of damage have you seen?



Appearance of typical fatigue fracture surface



- High cycle fatigue
- Low cycle fatigue
- Thermal fatigue
- Guillotine break
- Aging



Be prepared to what issues you are facing

Do not go to a measurement with “fingers in you ears”.

Half the job is done at the fika table

There are always an advantage to use multiple transducer types

- Multiple transducers help you see more complex situations.
- If the system has transient behaviour there are a lot of parameters you want to know about it.
 - Try to get as many as possible in the same measuring system.
 - If you just have one type use more than one position.
 - Use known information damage investigation, calculations, experiences, “control room chat”

To many thoughts how to measure

We always do like this!

- One type of transducer for all applications
- Measure continuous during known occasions
- Use periodic monitoring to measure the state of the system.
- This can work if there is a well known phenomena that is continuous

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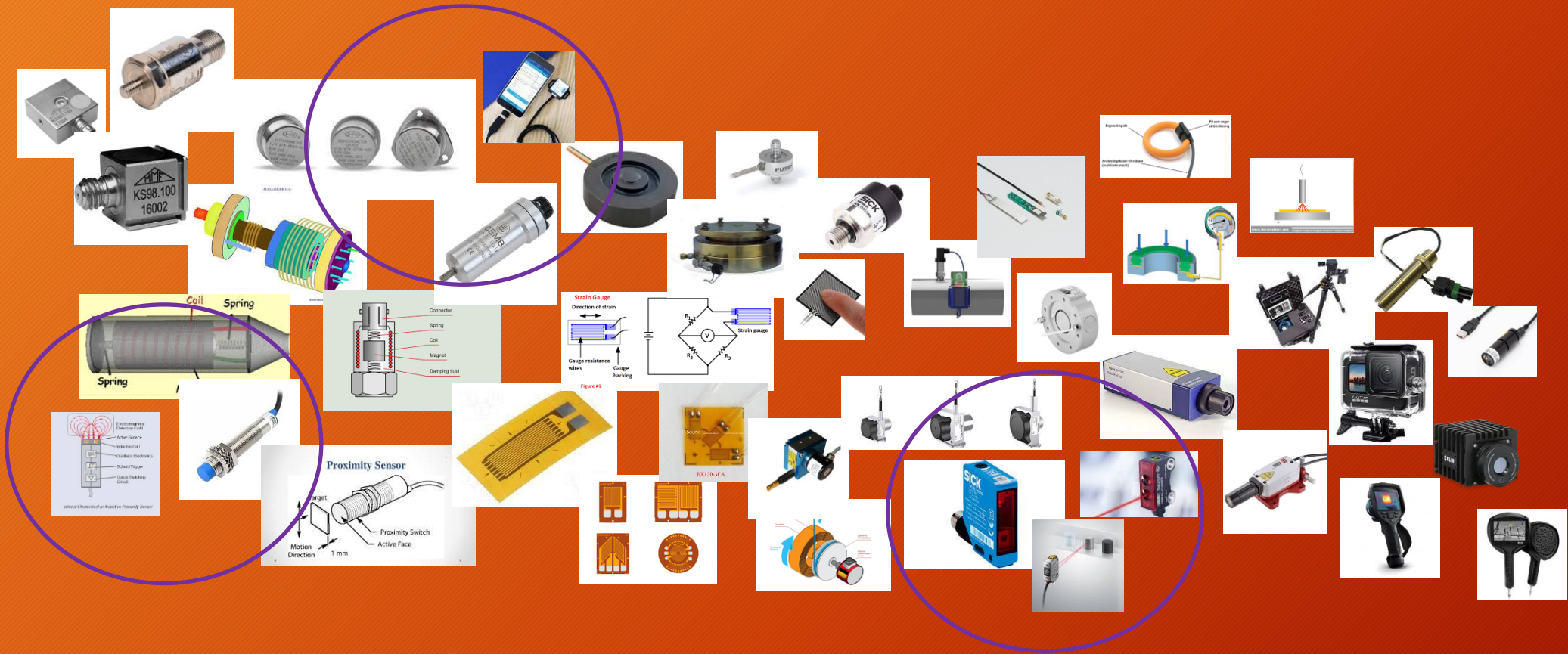
How will we get as much information as possible?

- Using different types of transducers from the beginning
- Searching all types of occasions, all time 24/7.
- It locks a measuring system for a long time
- This is a hard time evaluation but you can find the out of the box occasions



And
others

There are a lot of transducer types

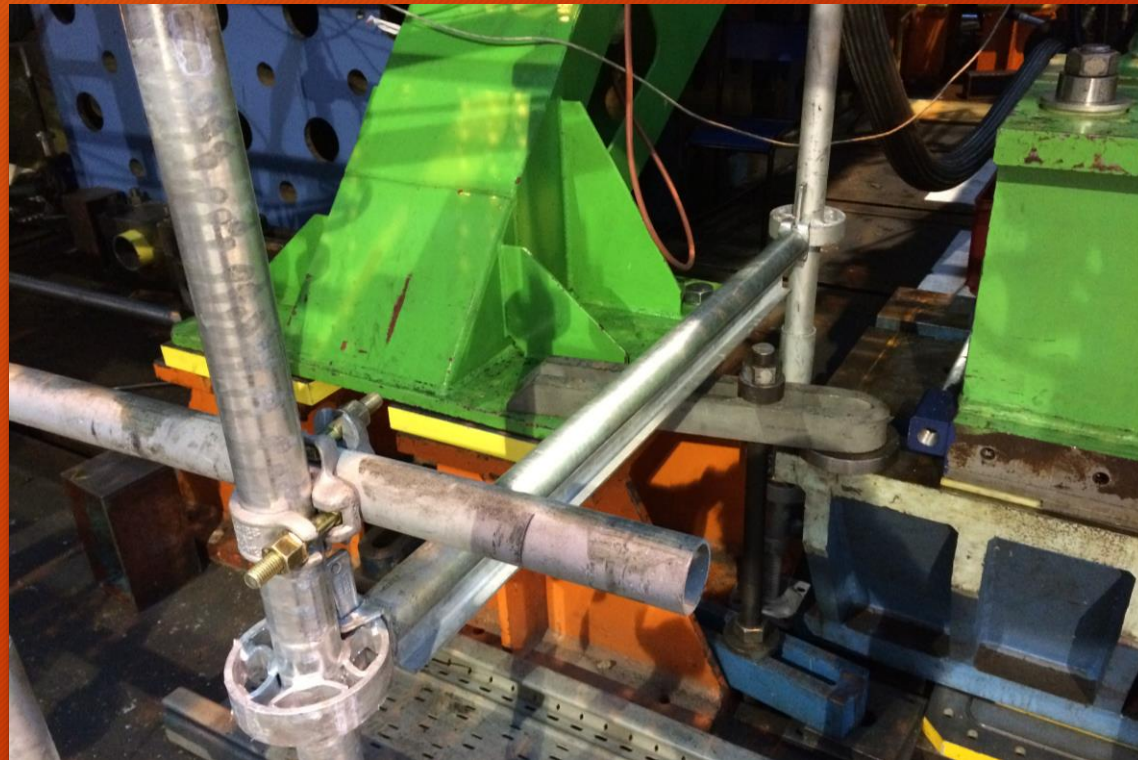


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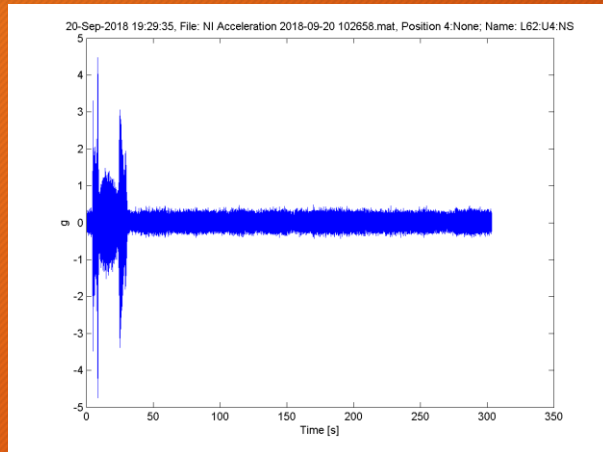
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How to choose?

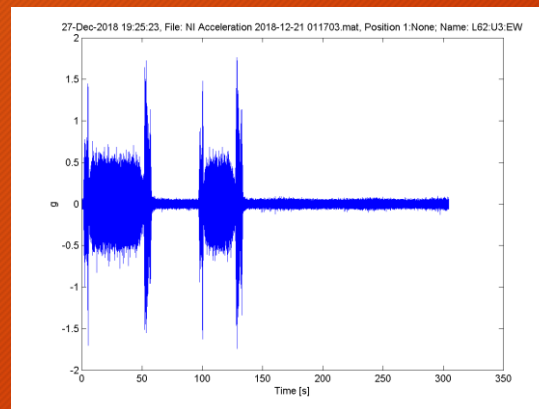
- What are expected?
 - Results
 - From the "customer"
- What purpose are there?
 - Damages
 - High vibration
 - Monitoring requirements
- If possible choose more than one type
 - Combinations can give another answer
 - Limitations



What's this?

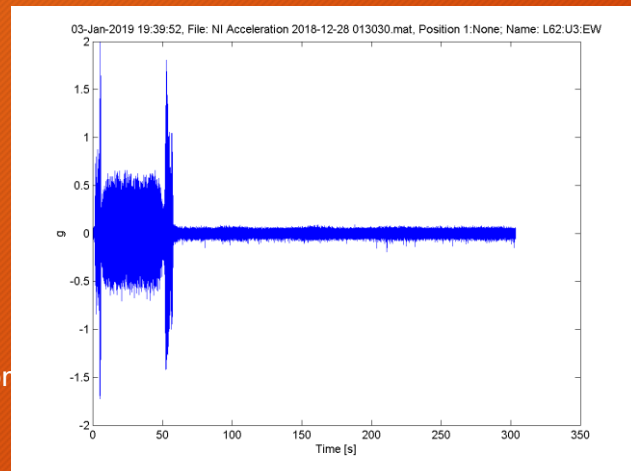


There were short ones



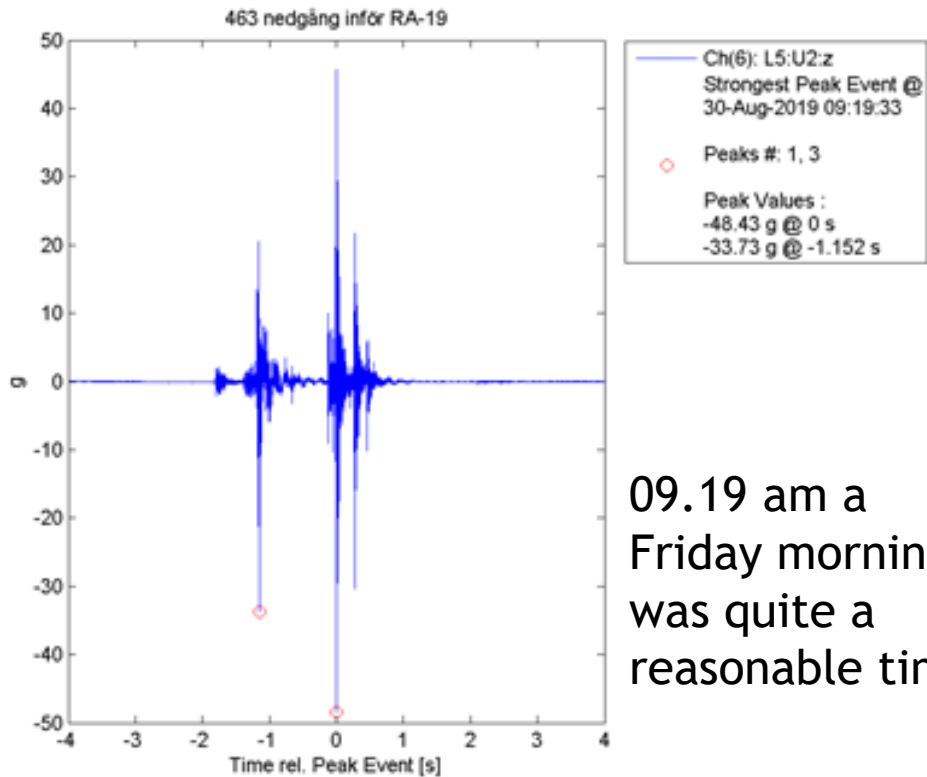
Double ones

This happened about 1am every Saturday morning

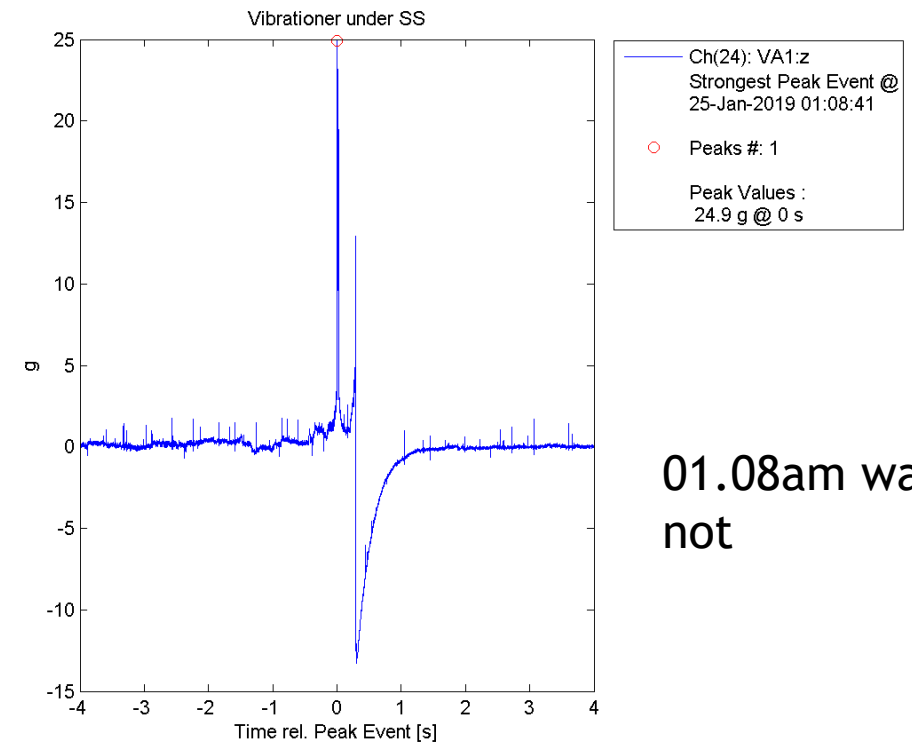


There were long ones even up to several minutes

Short compromising occasions

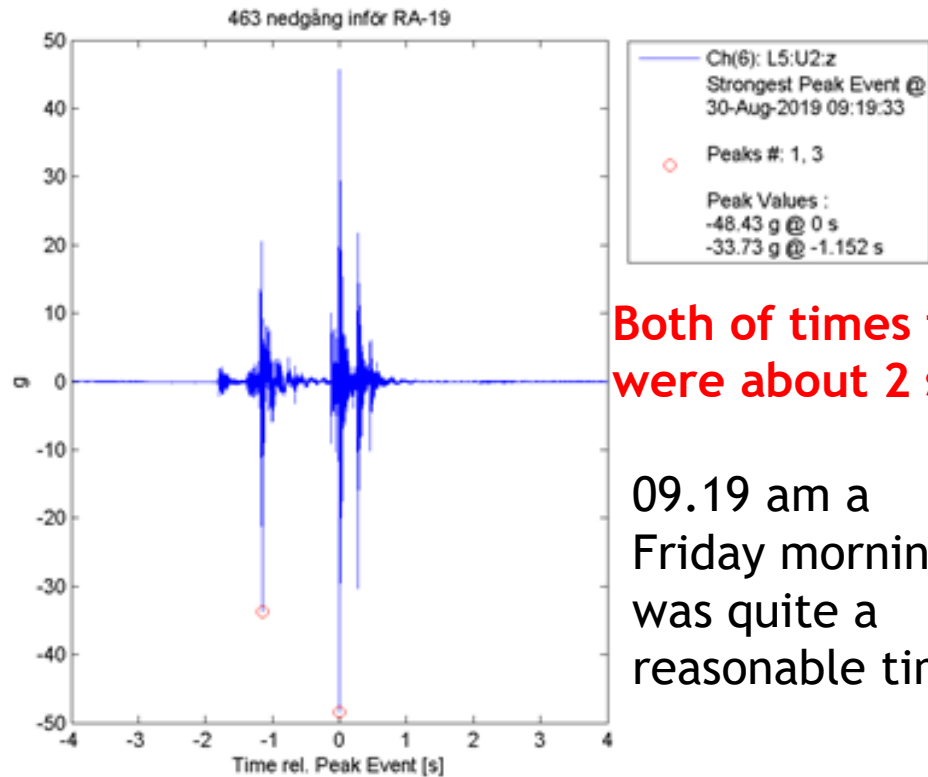


09.19 am a
Friday morning
was quite a
reasonable time



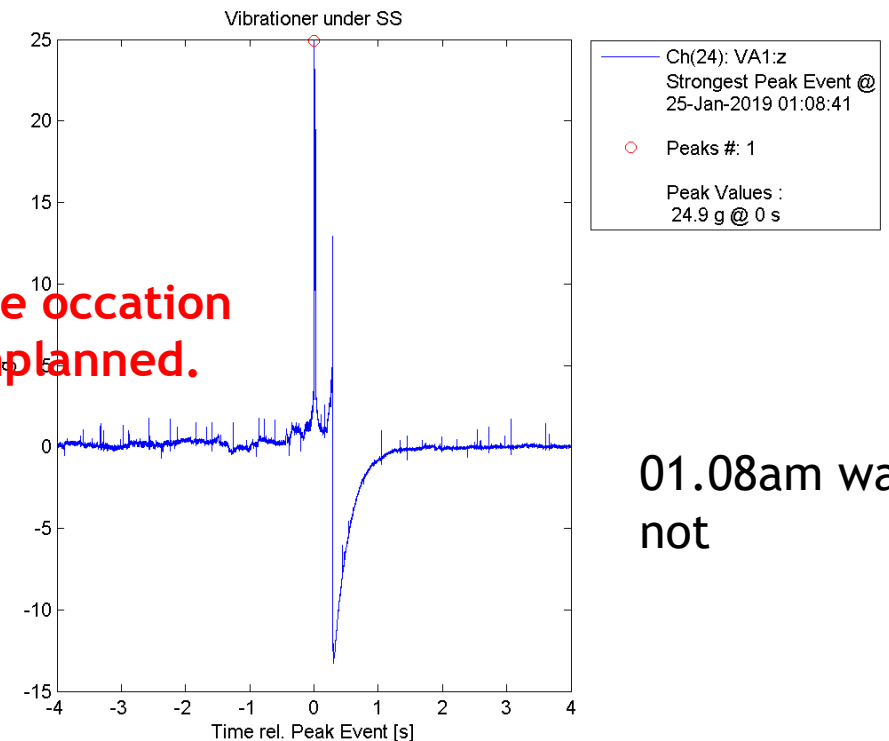
01.08am was
not

Short compromising occations



Both of times the length if the occation
were about 2 seconds and unplanned.

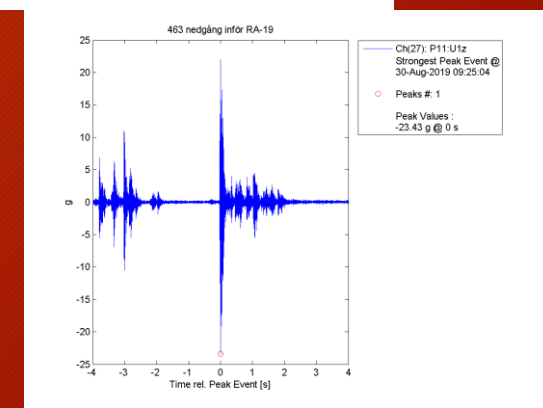
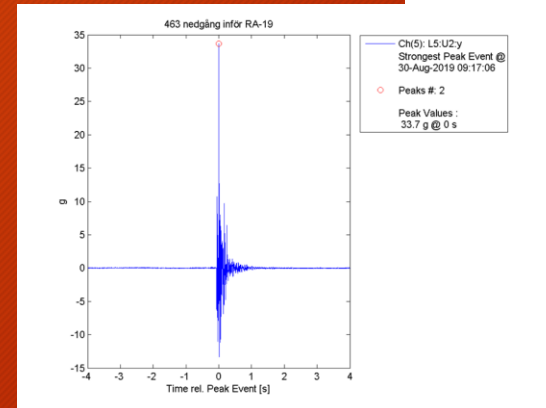
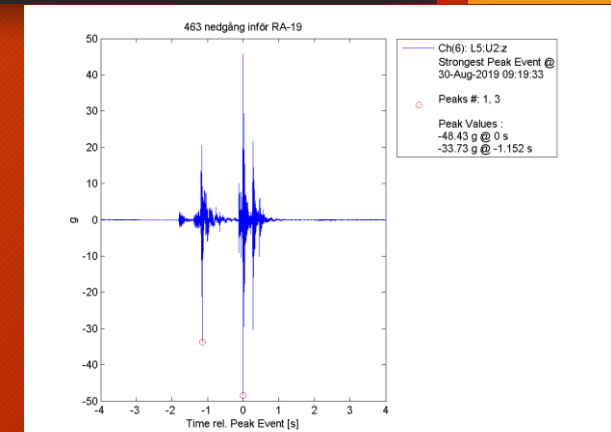
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Turbine stop

- Turbine stop from feed water pumps
 - In this case it was low load and only one of three feed water pump was in operation
 - There were three separate occasions that triggered high transients in the duration of eight minutes
 - 9.17 TS
 - 9.19
 - 9.25
 - The highest transient amplitudes are measured close to the pumps standing still.



Recommendation

- Measure continuous if possible
 - Shorter period, approximately a week, better than nothing
 - During a known test. Start the measuring well before test start
- Choose equipment and technics before you arrive BUT
 - Have a plan B
 - Take a little extra with you
- Beware of safety restrictions
 - This can affect your plan



Thank you

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