



Nuclear-Powered Direct Air Capture

Principles and Options

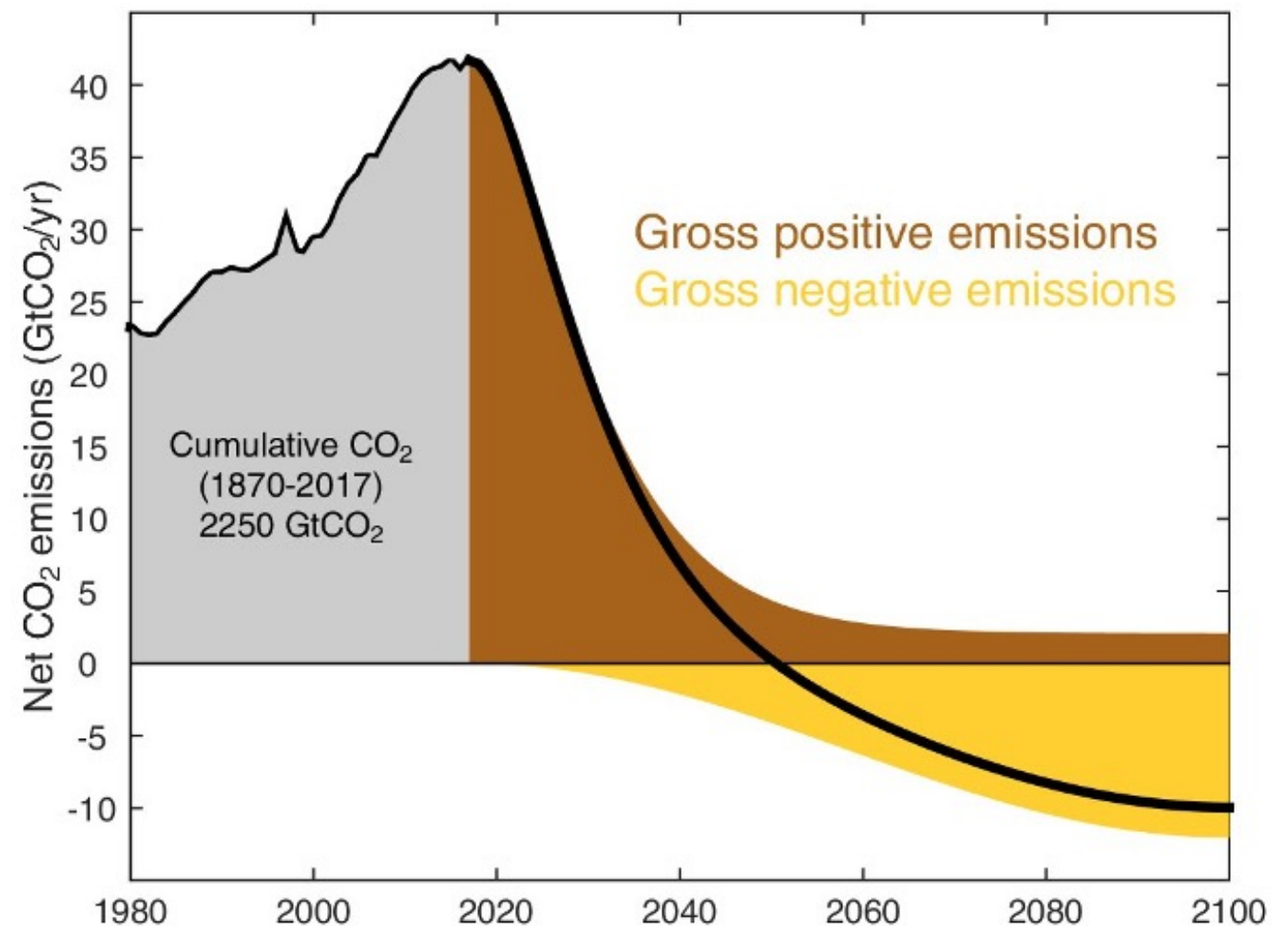
Dr Staffan Qvist — 2022/01/26

QC Ltd

Negative emissions

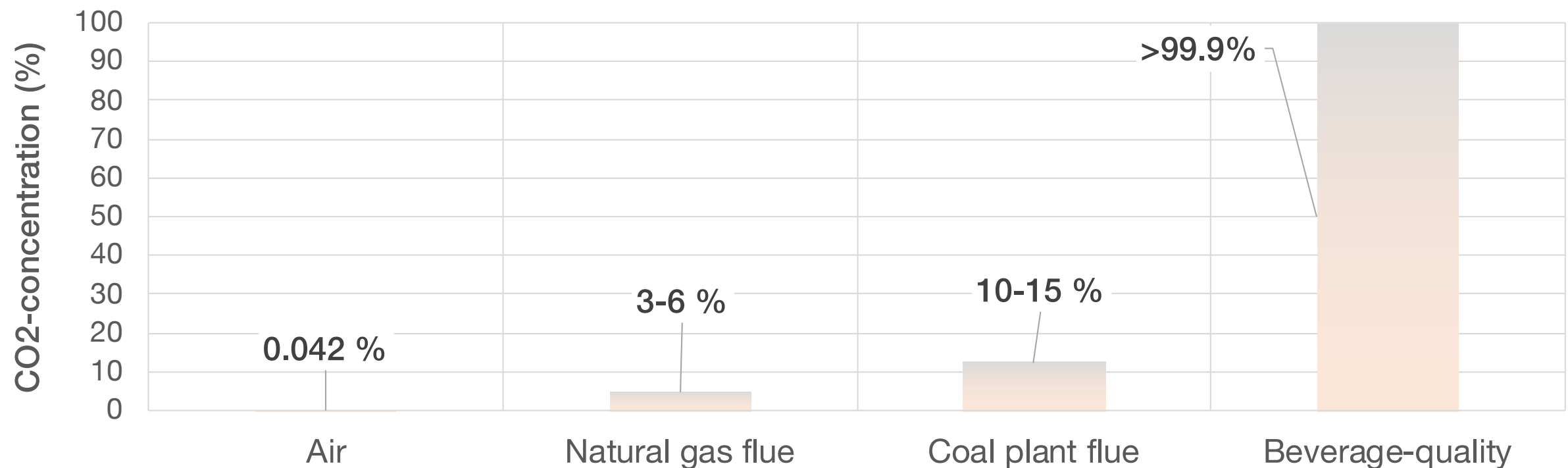
- Negative (CO₂) Emissions Technologies (NETs) are needed to keep the global average temperature increase below 2°C *in nearly all integrated assessment models*
- The scale of such negative emissions has been estimated to require extraction of up to 12 Gt of CO₂ per year after 2050 for a <2 °C warming limitation

Typical 1.5-2°C IAM model results

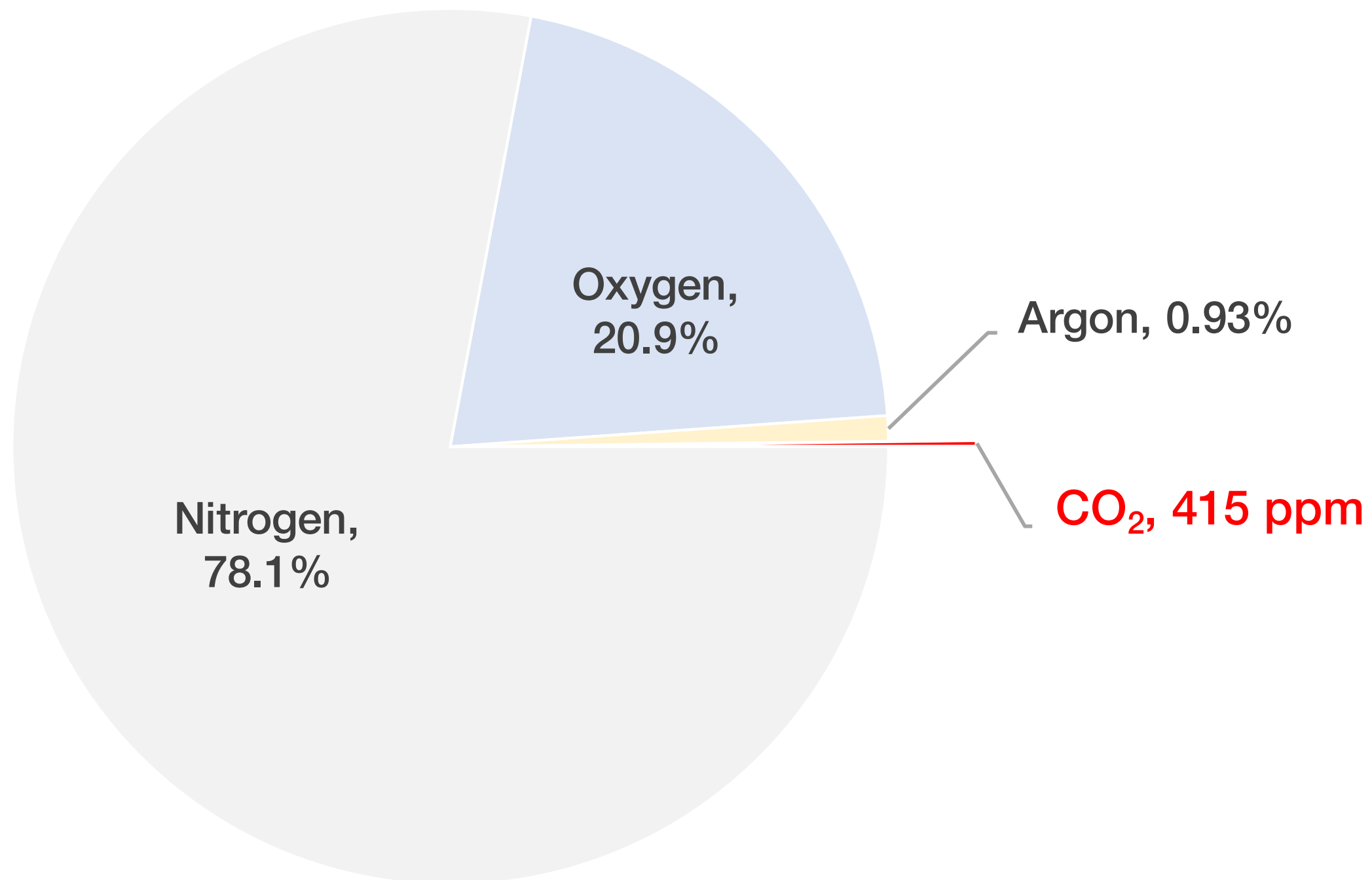


CCS and DAC?

- Direct Air Capture (DAC) can be seen as a type of CCS (Carbon Capture and Storage) or CCU (Carbon Capture and Utilization)
- DAC is distinguished by the concentration of CO₂ in the gas!

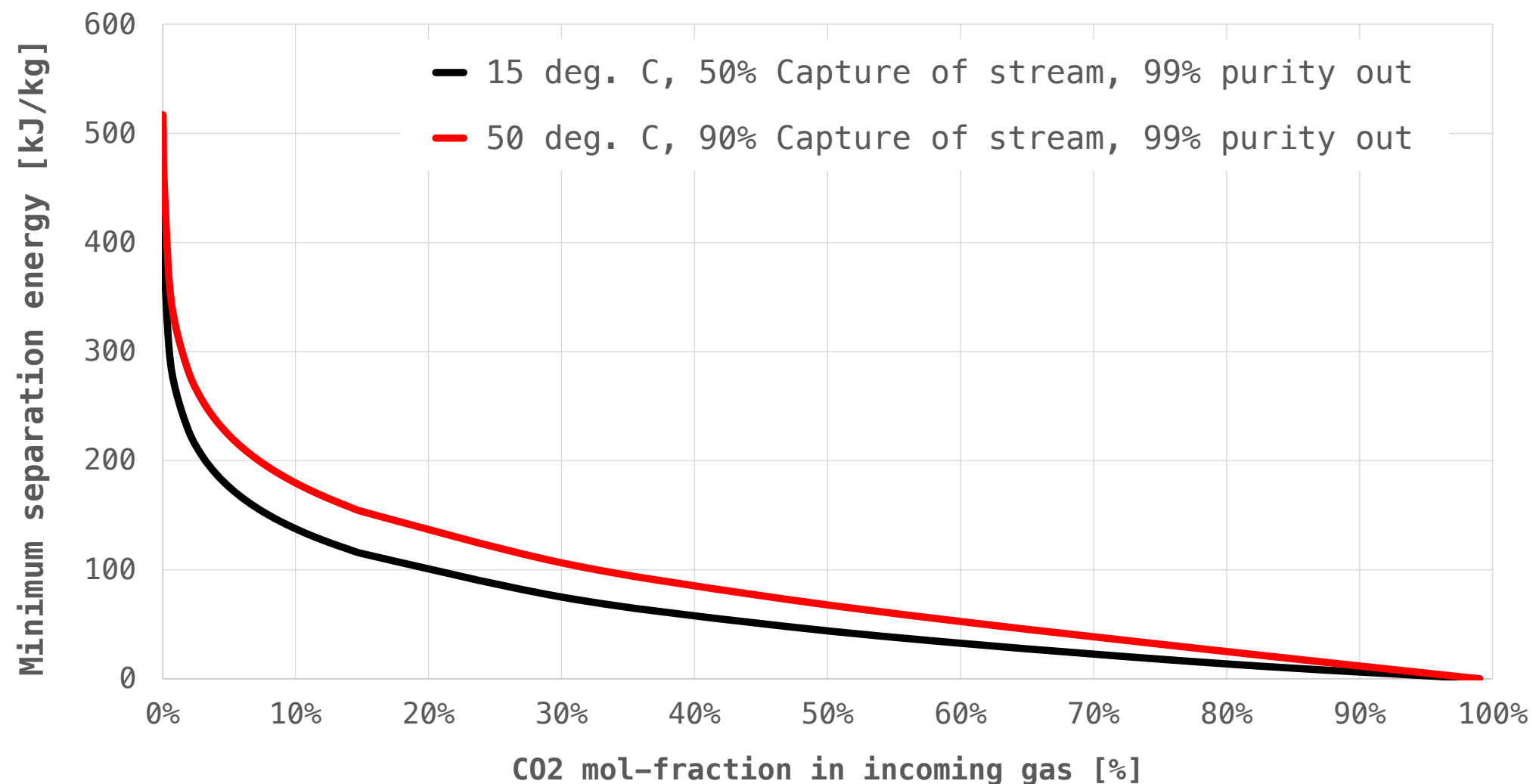


Atmospheric air



Theoretical separation energy

Minimum theoretical work required to separate CO₂ from air is ~3.5 times higher than from a coal plant flue stack, although concentration differs by a factor of 300

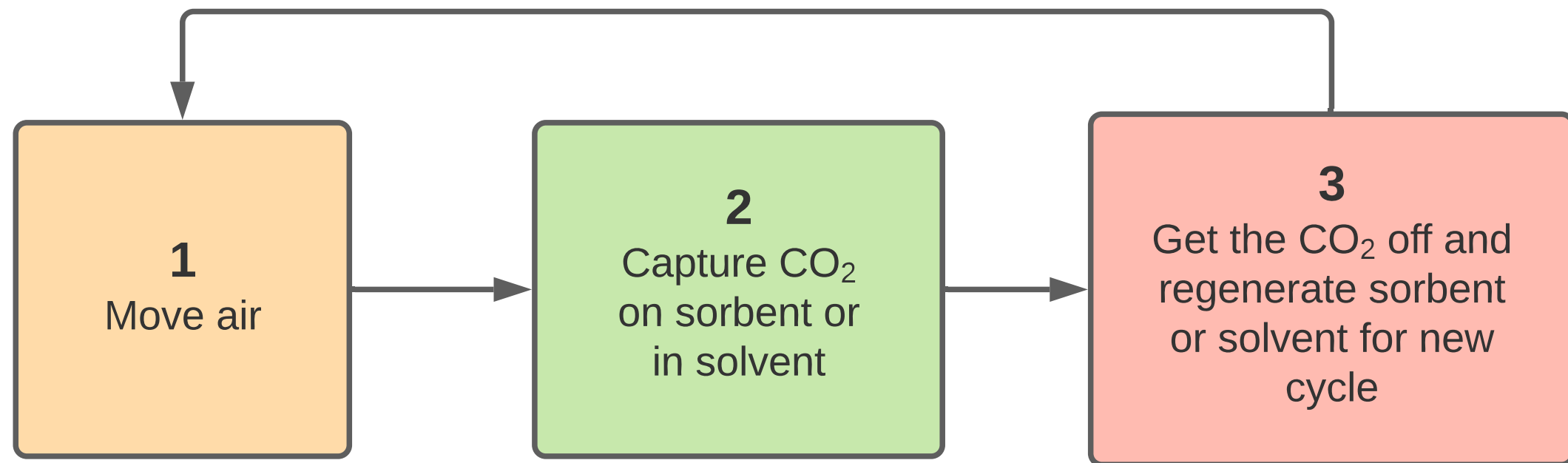


Siting options

- DAC, unlike flue gas carbon capture, is essentially location agnostic!
- However, ambient environmental conditions affect DAC performance, and the proximity to CO₂ storage/pipeline (if this is the preferred option) can be a determining factor economically
- Water vapour competes with CO₂ for the reactive sites on sorbents and adds to the thermal mass that must be heated during regeneration — dry air is better!

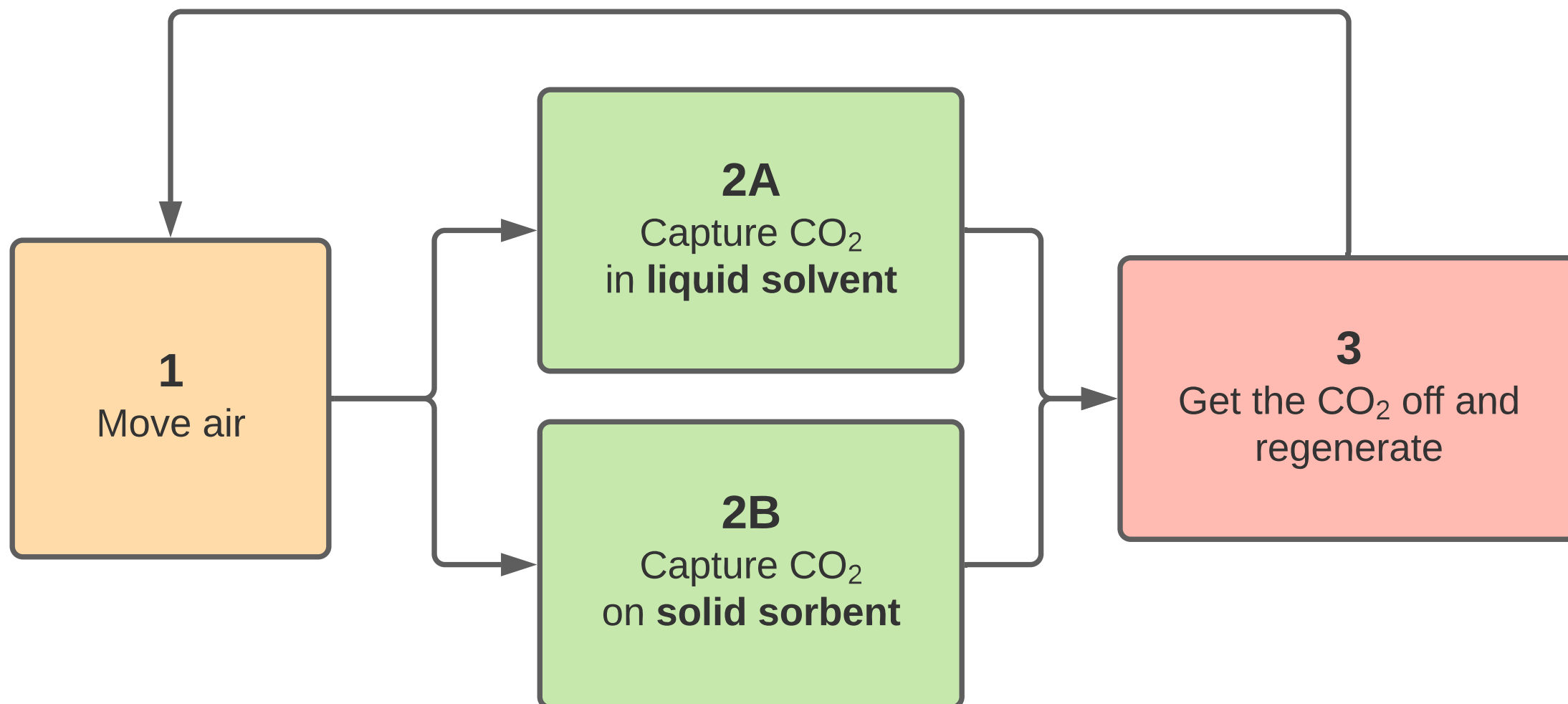
Principles of DAC

The core process has three main steps



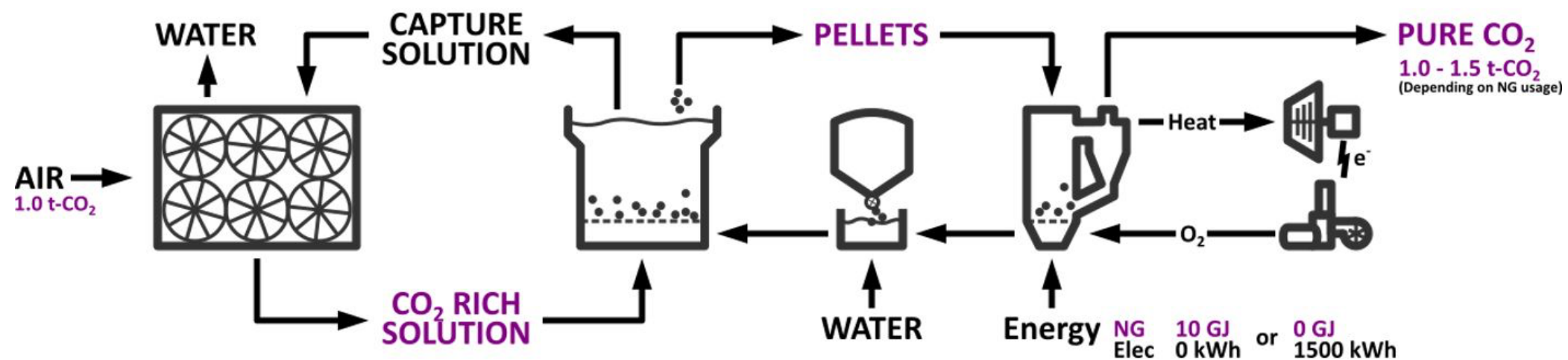
Types of DAC systems

On the very highest level, there are two pathways:
Liquid systems (2A) and Solid systems (2B)



Liquid solvent DAC system

- Solution spearheaded by Carbon Engineering (Canada).
- Regeneration cycle requires heat at 900°C in the calciner for the decomposition of CaCO_3 into CaO and CO_2 .
- Limits the full heat integration options with nuclear energy



AIR CONTACTOR
Pulls in air and passes it over a potassium hydroxide solution to capture CO₂ in a carbonate salt.

PELLET REACTOR
Removes the carbonate from the capture solution into small pellets. The capture solution is reused in the AIR CONTACTOR.

SLAKER
Hydrates recycled pellets which are reused in the PELLET REACTOR.

CALCINATOR
Heats the carbonate containing pellets to release CO₂ gas for long-term storage.



Nuclear + Liquid solvent DAC system

Powered by:

- Electrical power (source-agnostic, so technically uninteresting)
or..
- Heat supplied by high temp gas cooled reactor (HTGR)
 - 950°C coolant outlet could enable 900°C process heat supply



AVR, 1967-1988
950°C out

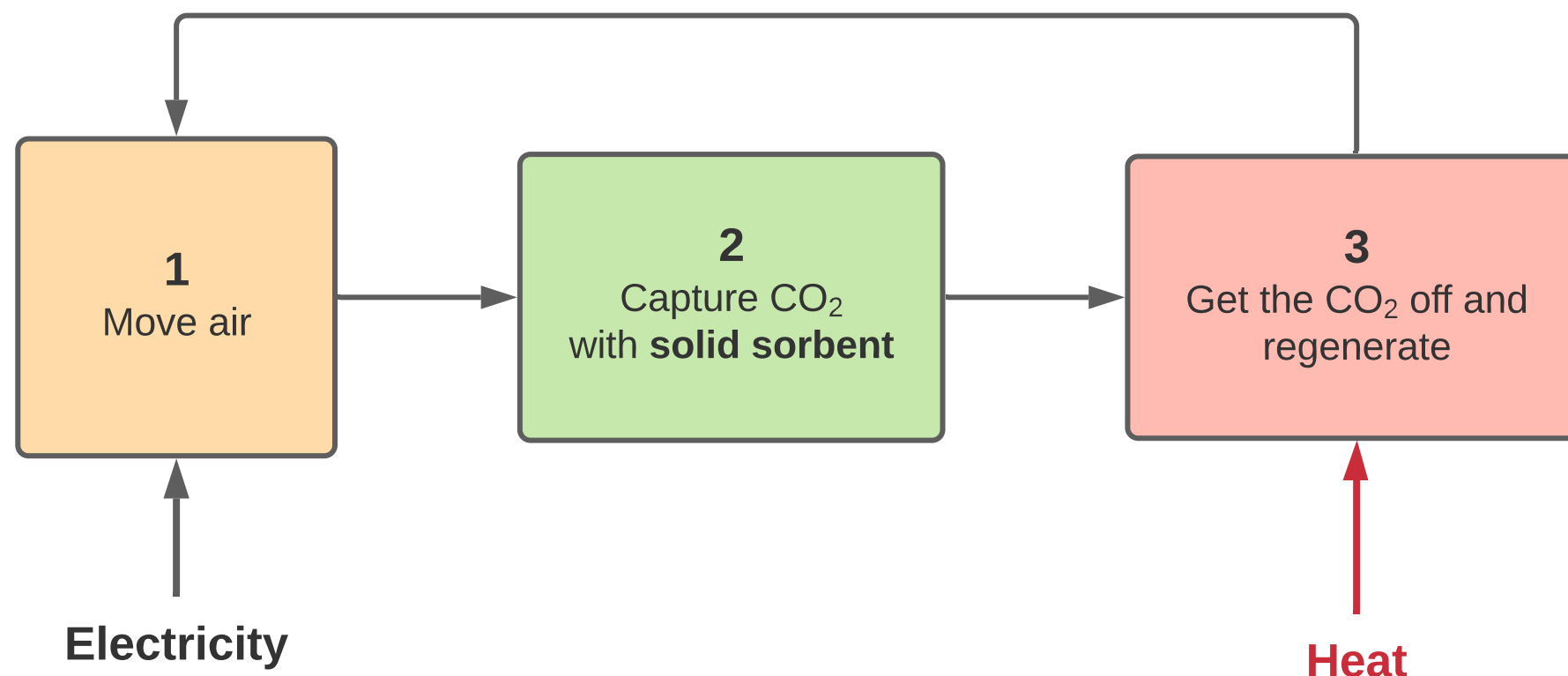


HTTR, 1999 -
950°C out

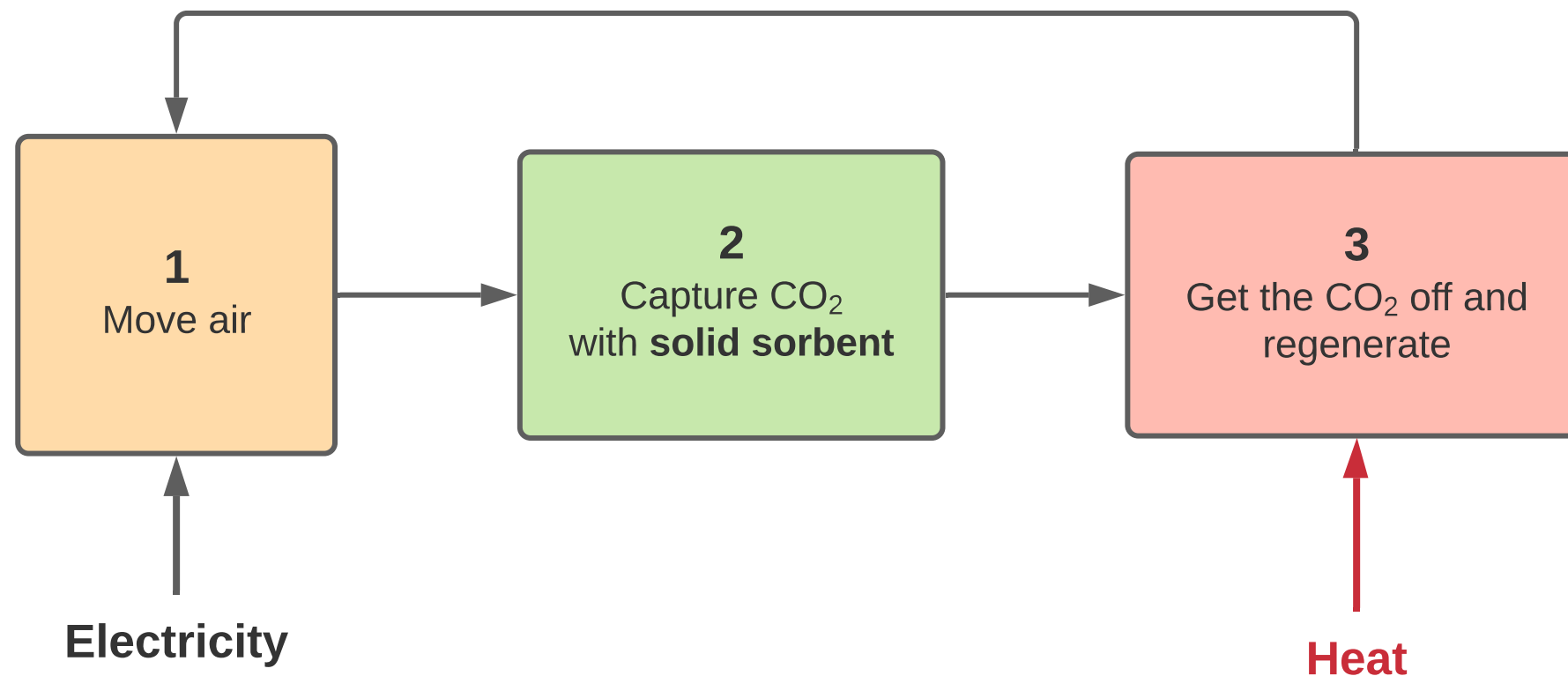


HTR-PM, 2021-
750°C out now (900+ possible)

Low-temperature solid adsorbent DAC



Energy requirements today



Electrical fans

0.5-1.0 MWh
per ton CO₂-captured

100-130°C

2-3.5 MWh
per ton CO₂-captured

The diagram illustrates the flow of air during the adsorption phase of CO2 capture. It starts with a **Fan/Blower** (represented by a three-lobed propeller icon) that draws in **ELECTRICITY** (indicated by a downward arrow). The air then enters a container labeled **Incoming air**, which contains **Nitrogen, Oxygen, Argon etc..** (in a grey section) and **CO₂** (in a red section). This air passes through a **Valve** (labeled **Open** with a valve icon) into a blue box labeled **Adsorption**, where **CO₂ is captured in sorbent**. Finally, the air passes through another **Valve** (labeled **Open** with a valve icon) into a container labeled **CO₂-depleted air**, which also shows a red section at the bottom.

The diagram illustrates the depressurization process. A blue box labeled "Depressurization Emptying out unit atmosphere" is the central component. To its left, a pipe with a closed valve (indicated by a red 'X') is labeled "Closed". Below the box, the word "HEAT" is written in red. To the right of the box, there are two parallel pipes. The top pipe has a closed valve (red 'X') labeled "Closed". The bottom pipe has an open valve (green circle) labeled "Open". This open pipe leads to a "Vacuum Pump", represented by a grey circle. An arrow labeled "ELECTRICITY" points down to the vacuum pump. An arrow points from the vacuum pump to the right, labeled "Air in capture unit relased to atmosphere".

Diagram illustrating the process of releasing CO₂ from the sorbent:

- The central unit is labeled "Sorbent heating To release CO₂ from sorbent".
- A red arrow labeled "HEAT" points down into the unit.
- The unit is connected to a "vacuum Pump" on the right via two parallel lines, each with a "Closed" valve.
- A single line on the left also has a "Closed" valve.

ELECTRICITY

CO₂-rich stream

CO₂

Purification, Compression, Liquefaction Processing, Transport etc.

ELECTRICITY

CO₂ extraction pump

Open

Emptying out To extract concentrated CO₂

Closed

Closed

The diagram illustrates the active cooling cycle for sorbent regeneration. A central rectangular box is divided horizontally: the top half is light blue and labeled "Sorbent cooling", while the bottom half is light red and labeled "To enable a new cycle of capture". A blue arrow points down to the top of the box from the text "(ACTIVE COOLING)" above it. To the left of the box, a grey pump is connected to a horizontal line. This line has two valves: a green valve labeled "Open" and a red valve labeled "Closed". To the right of the box, a similar horizontal line has a green valve labeled "Open" and a red valve labeled "Closed", which is connected to another grey pump.

Nuclear (LWR) powered DAC options

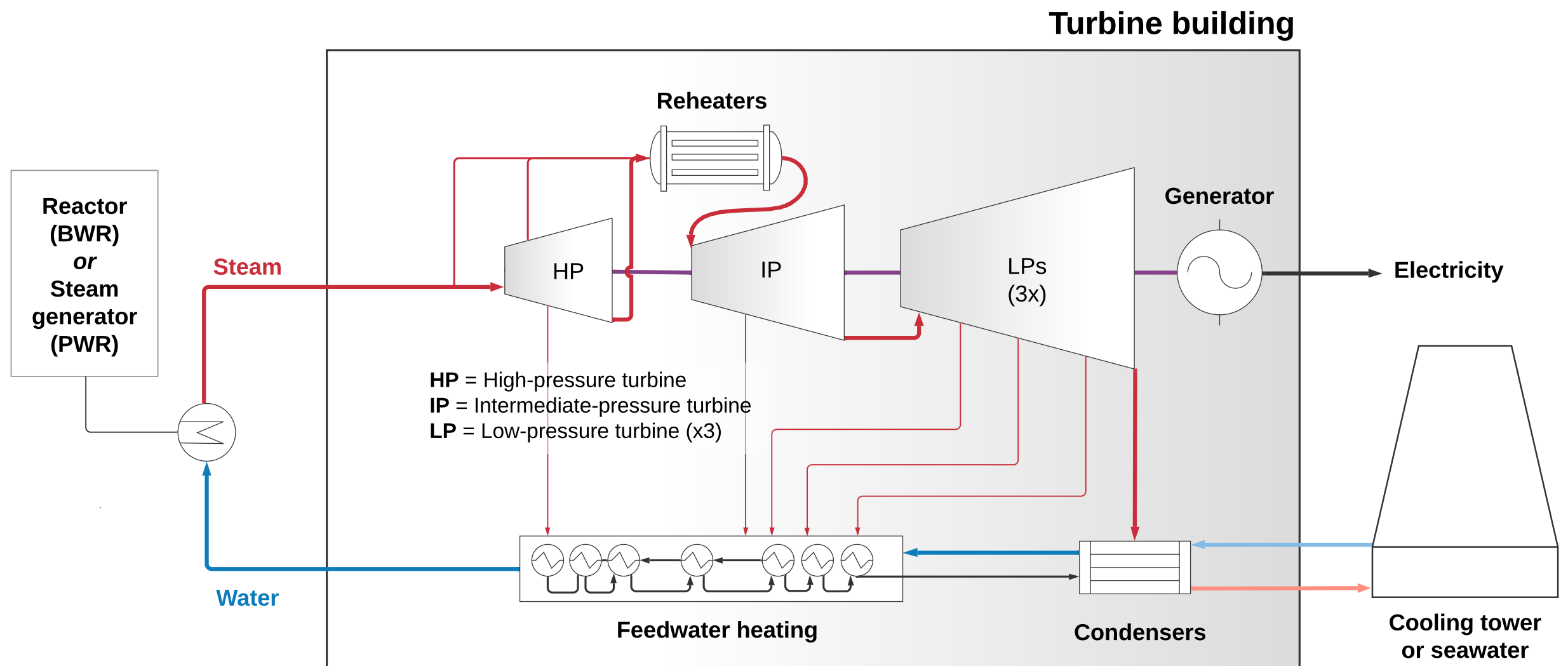
1. Power current-day solid-adsorbent DAC systems

- ✓ Use steam extraction to regenerate solvents

2. Optimize DAC for nuclear energy integration

- ✓ Use steam extraction to regenerate solvents
- ✓ Move air through system using waste heat

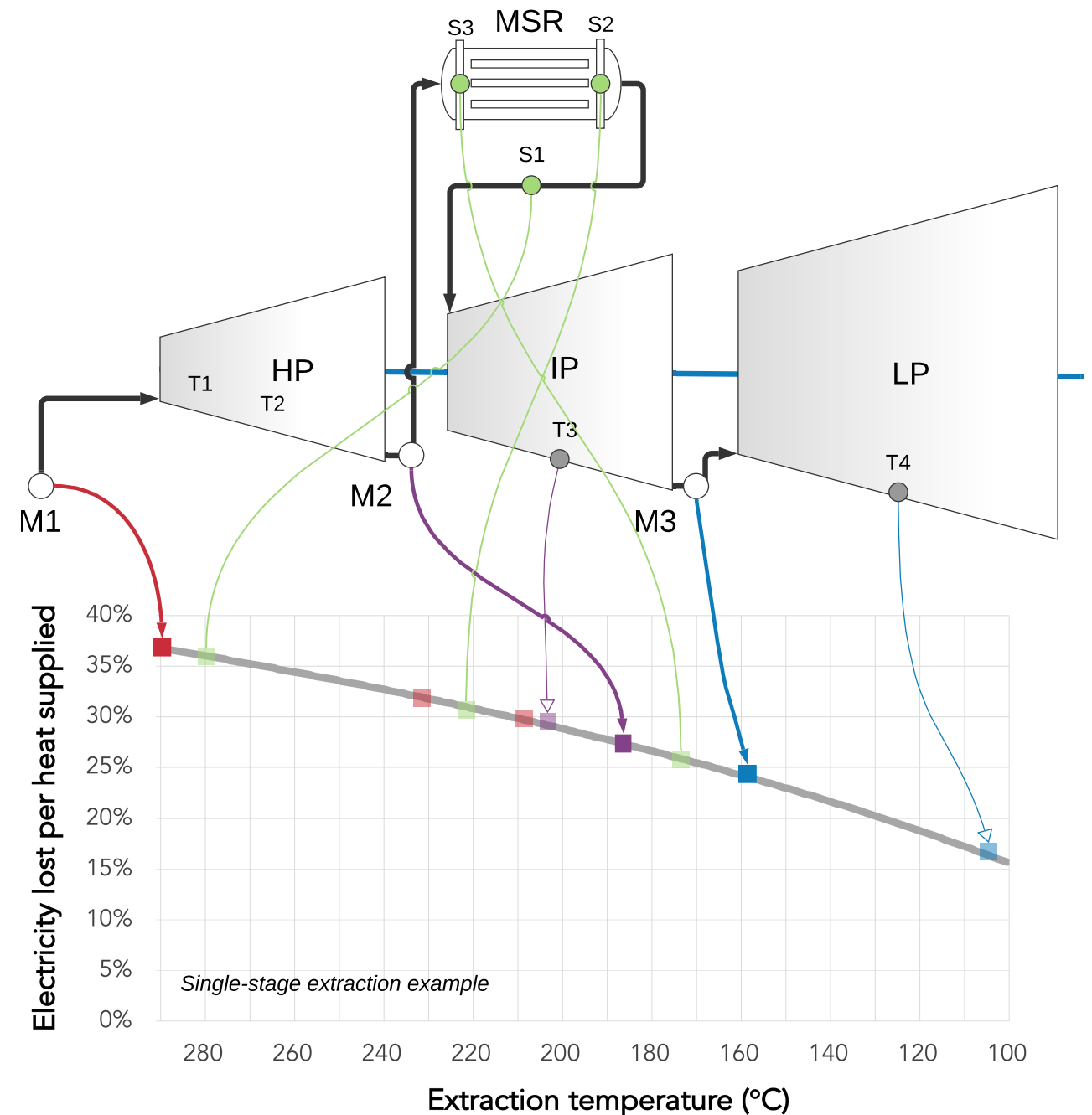
Extracting LWR heat for DAC regeneration



Extracting LWR heat for regeneration

Extracting steam reduced electricity output by:

$$P = \eta \times \frac{(T_R - T_C)}{(T_R + 273.15)}$$

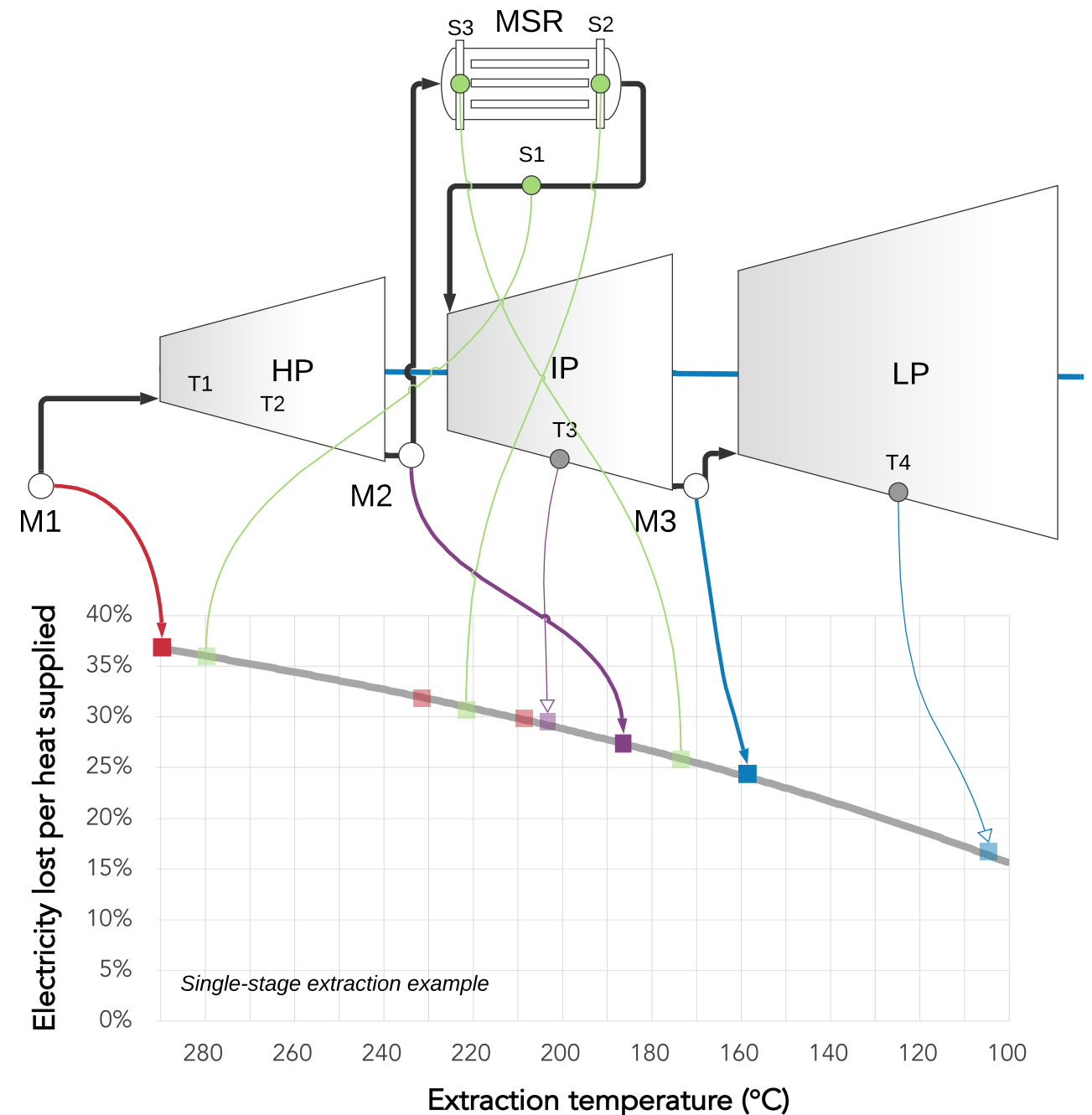


Extracting LWR heat for regeneration

Extracting steam reduced electricity output by:

$$P = \eta \times \frac{(T_R - T_C)}{(T_R + 273.15)}$$

$$P = 0.789 \times \frac{(T_R - 35)}{(T_R + 273.15)}$$



Extracting LWR heat for regeneration

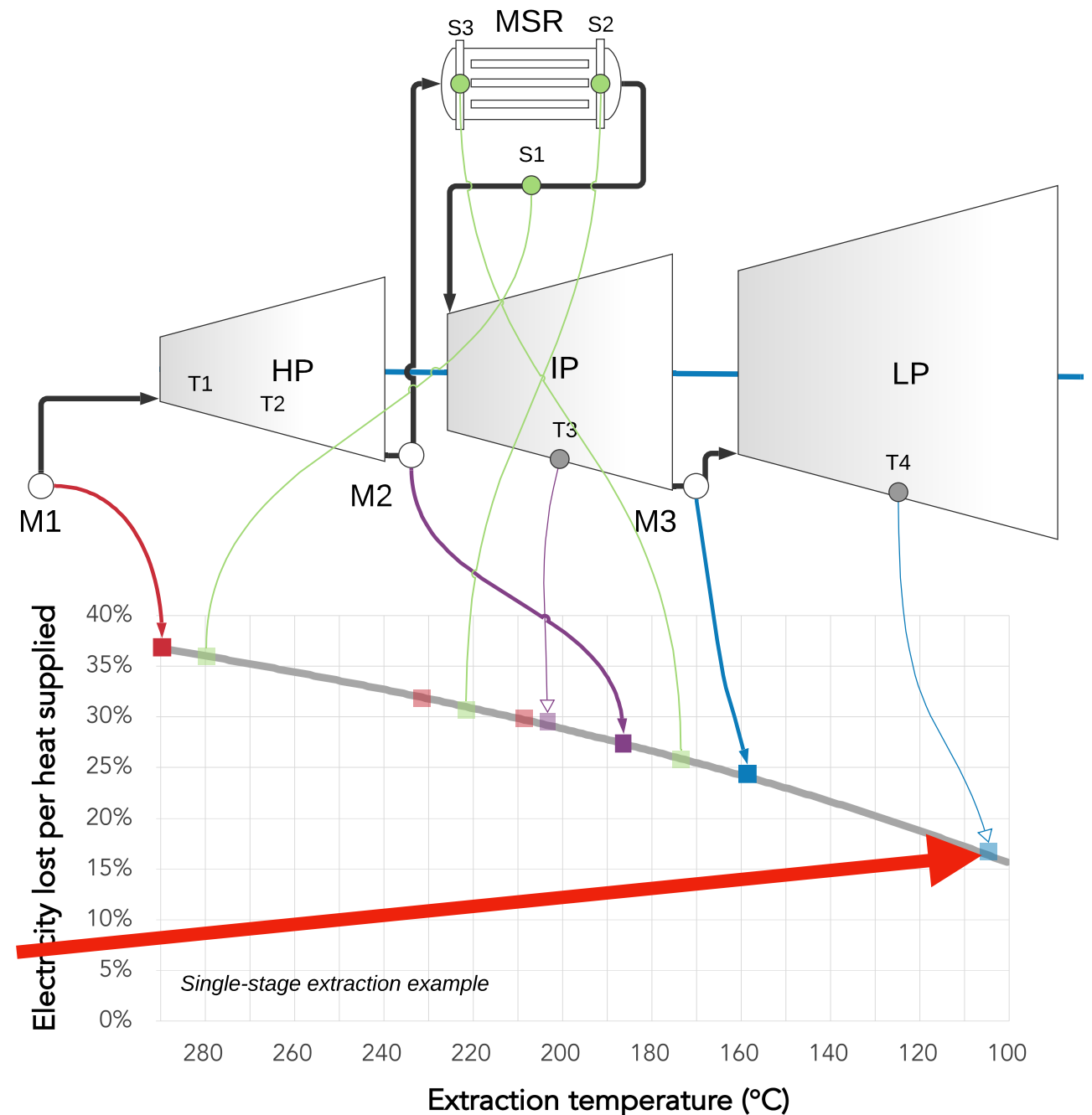
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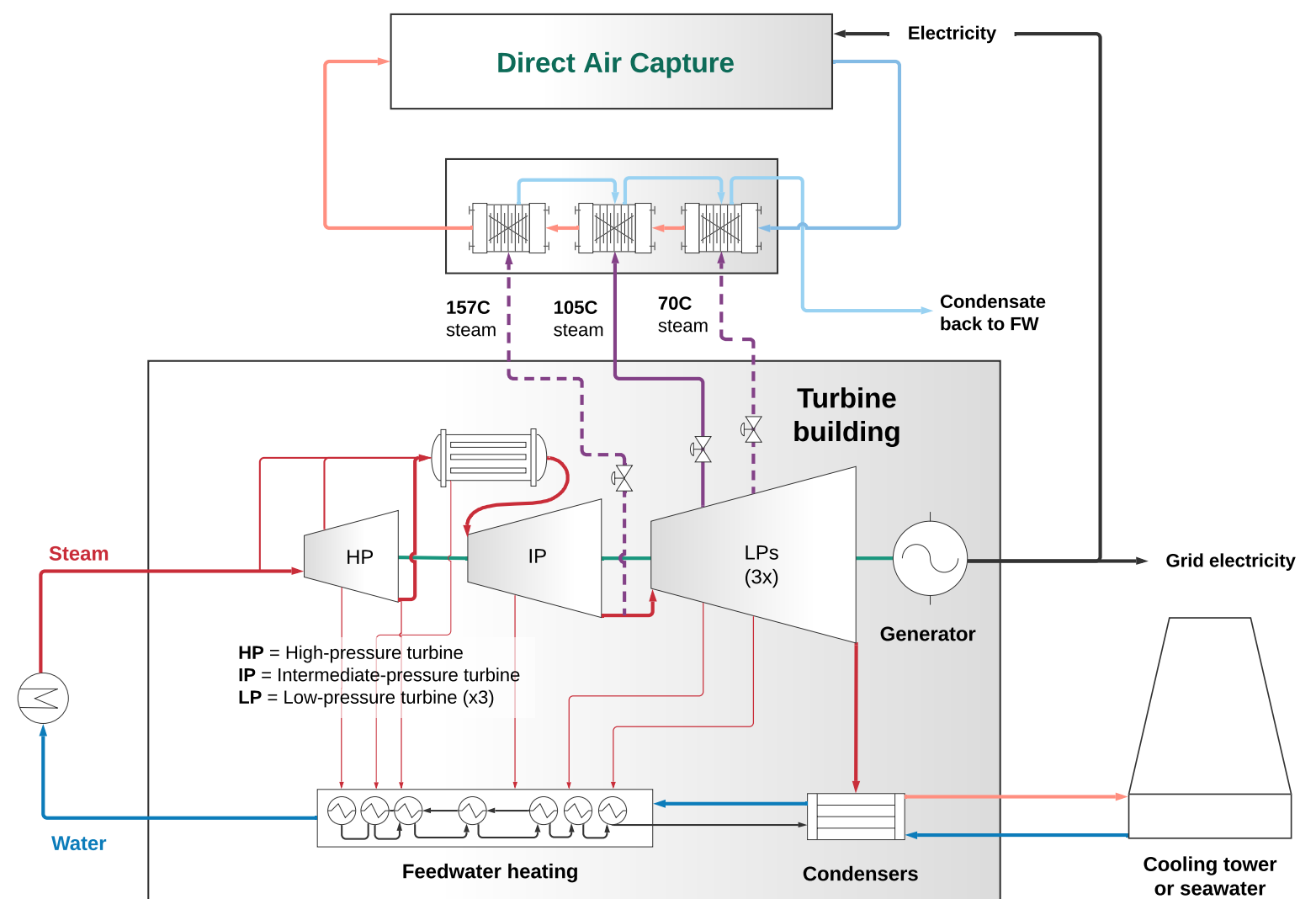
$$P = 0.789 \times \frac{(105 - 35)}{(105 + 273.15)} = 0.146$$

1/7th MWh lost per 1 MWh heat supplied!



LWR-powered DAC system

- Extract heat out to external condensing HX, return condensate to FW system
- A 3-stage extraction system means losing 0.15 MWh of electricity for each MWh of heat supplied (at 120C)
- Easiest 1-stage extraction point is at the cross-over before the low-pressure turbine stage (0.25 MWh/MWh lost)
- Up to 10% of thermal power can be extracted with minor modifications



Optimized nuclear-DAC system

PROCESS & SORBENT DEVELOPMENT



PROTOTYPE ENGINEERING
& CONSTRUCTION



HOST, UTILITY SUPPLY
& PROJECT MANAGEMENT

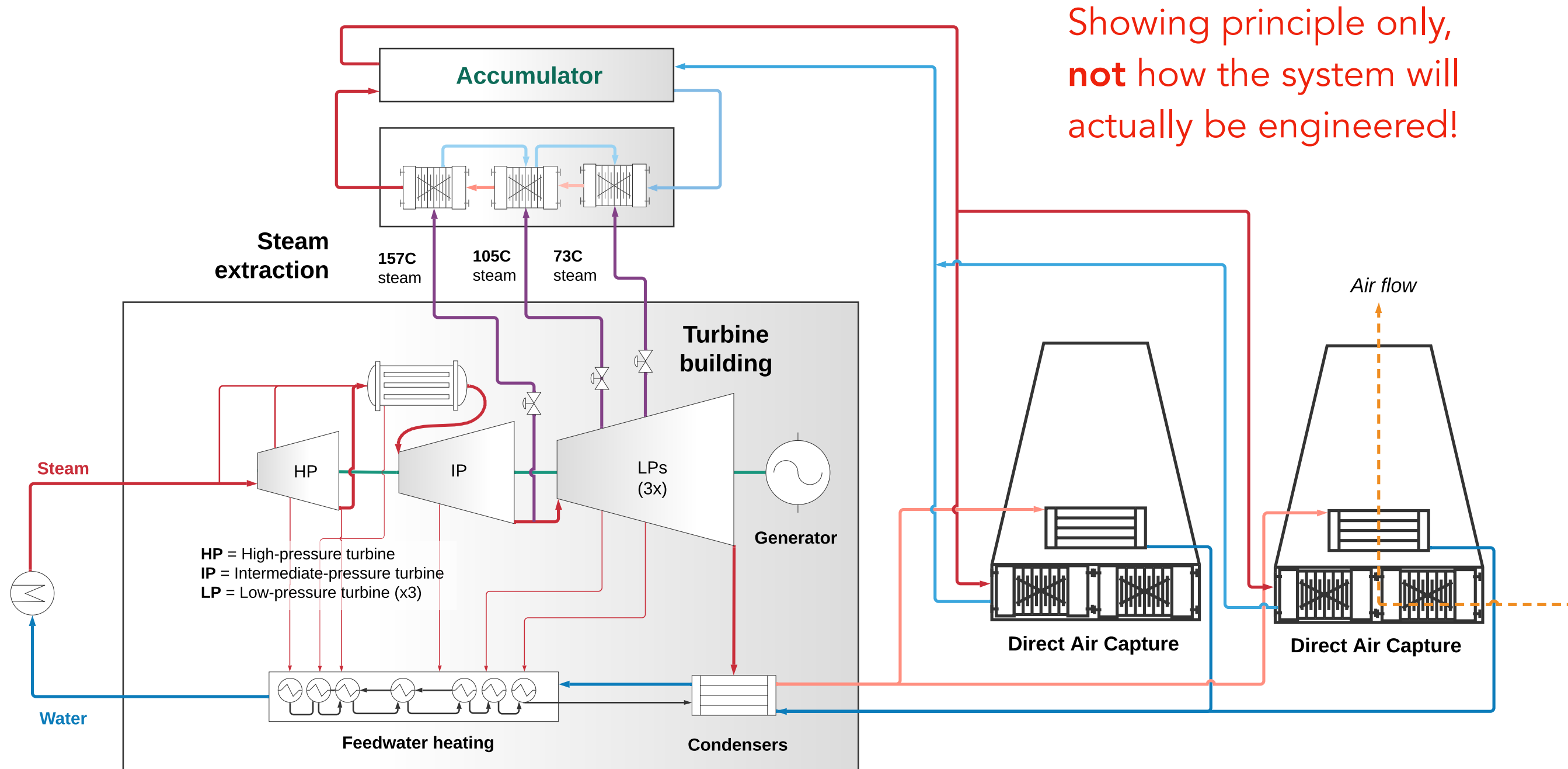
INDUSTRIAL MANUFACTURING



COMMERCIALIZATION

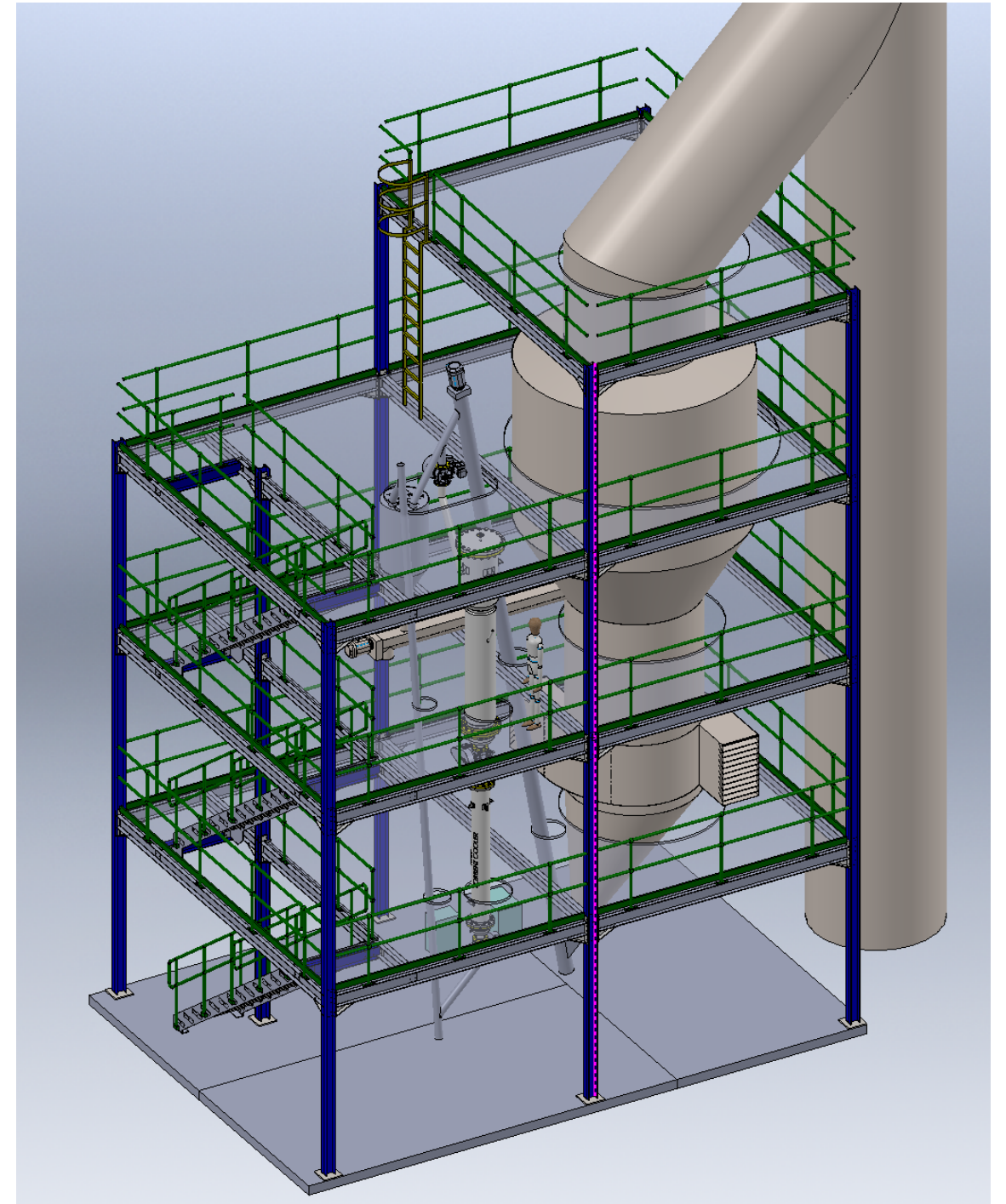
ATKINS

Principle of integration



Engineering development

- 100 ton CO₂/year plant designed
- Electrical heating as stand-in for nuclear co-generation for heat to move air (mimicking condenser cooling heat) and heat to regenerate (mimicking steam extraction)
- Winner of UK Government DAC competition, £250k grant first phase, second (build) phase £2m
- **A new standard SMR condenser cooling system?**



DAC economic basics

Three main components

- Cost of DAC equipment
- Cost of electricity supply
- Cost of heat supply

Assumptions for cost of DAC equipment

Year	2020	2030	2040	2050
CAPEX _{DAC} (€/tonCO ₂ /y)	730	338	237	199
OPEX _{FIX} (€/tonCO ₂ /y)	29.2	13.5	9.5	8.0
OPEX _{var} (€/tonCO ₂)	3	3	3	3

DAC cost floor

Assumptions for *levelized* cost of DAC equipment alone €/tonCO₂ (w. no utility supply) by capacity factor

Year	2020	2030	2040	2050
CF = 100% (Theoretical floor)	94.8	45.5	32.8	28.1
CF = 95% (Grid power)	99.7	47.7	34.4	29.4
CF = 85% (Nuclear dedicated)	111.0	53.0	38.1	32.5
CF = 35% (Onshore wind dedicated)	265.4	124.4	88.2	74.6
CF = 12% (Nordic PV dedicated)	768.3	357.2	251.6	212.0

Optimized nuclear DAC economics

Reference cost of electricity supply (no modifications):

- €50/MWh

Cost of DAC electricity supply

- $20 \text{ kWh/tonCO}_2 * €55/\text{MWh} \approx €1/\text{tonCO}_2$

Cost of DAC heat supply

- Electricity Opportunity Cost +
 - Terminal equipment & Upgrades at plant +
 - High + Low Temp Heat Transport Equipment Cost +
 - Additional operational expenses
- $\approx €17/\text{tonCO}_2$

Comparison economics

Electricity from grid or dedicated renewables

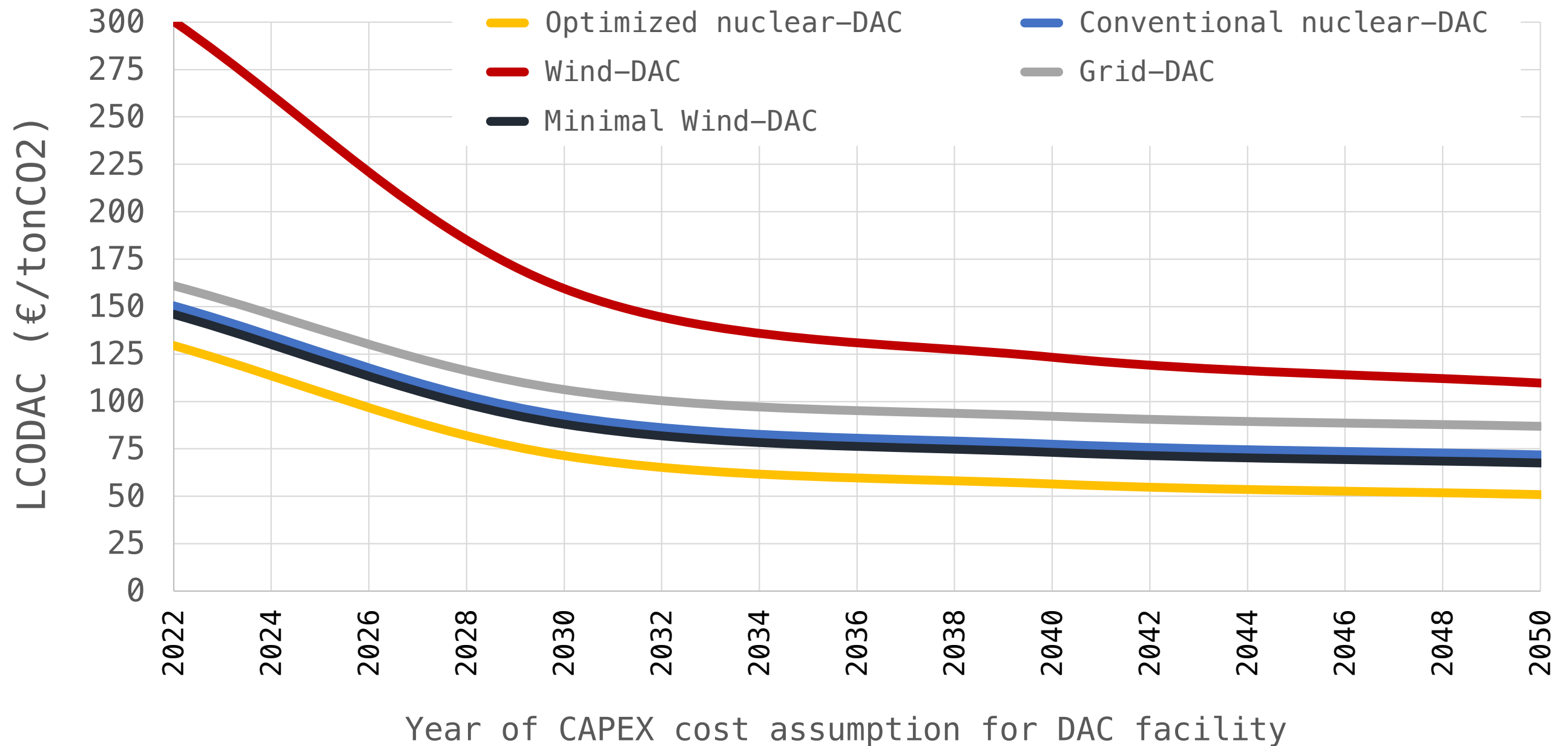
Cost of DAC electricity supply

- $0.4 \text{ MWh/tonCO}_2 * €25-40/\text{MWh} \approx €10-16/\text{tonCO}_2$

Cost of DAC heat supply through advanced heat pumps

- $1 \text{ MWh/tonCO}_2 * €25-40/\text{MWh} \approx €25-40/\text{tonCO}_2$

Comparative economics



Conclusions

- A nuclear plant can reach capture cost of $\sim \text{€}50/\text{tonCO}_2$, with life-cycle CO_2 -emissions of $-160 \text{ gCO}_2/\text{kWh}$
- Even at *assumed* far higher LCOE, a nuclear-DAC system has lower LCOD than systems powered by VRE or grid
- A nuclear-optimized DAC system is being developed & commercialised currently, if successful could eventually become a standard SMR condenser cooling system
- Captured CO_2 can form basis (alongside H_2 from effect water electrolysis) for synthetic hydrocarbons



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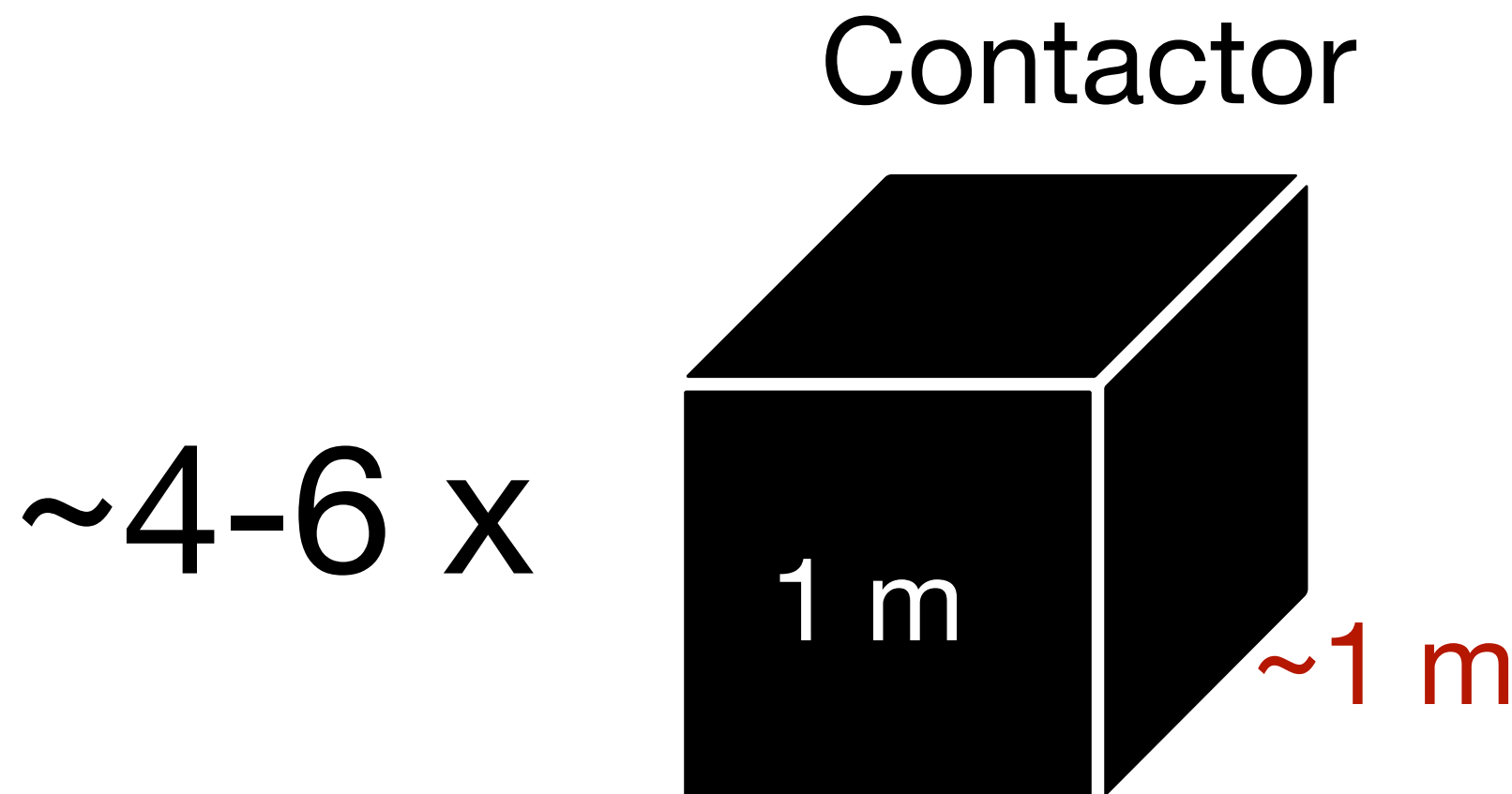
Sorbents

- Sorbents are chemicals that contain molecules that have affinity for CO₂ and bind to it. Monoethanolamine (MEA) and other amines have been used commercially for this for decades.
- Four main factors determine DAC sorbent suitability:
 - Reactivity (how effectively does it bind CO₂)
 - Regeneration energy
 - Degradation rate
 - Cost & Availability
- Difficult trade-off regarding all four factors!

How large are “contactors”?

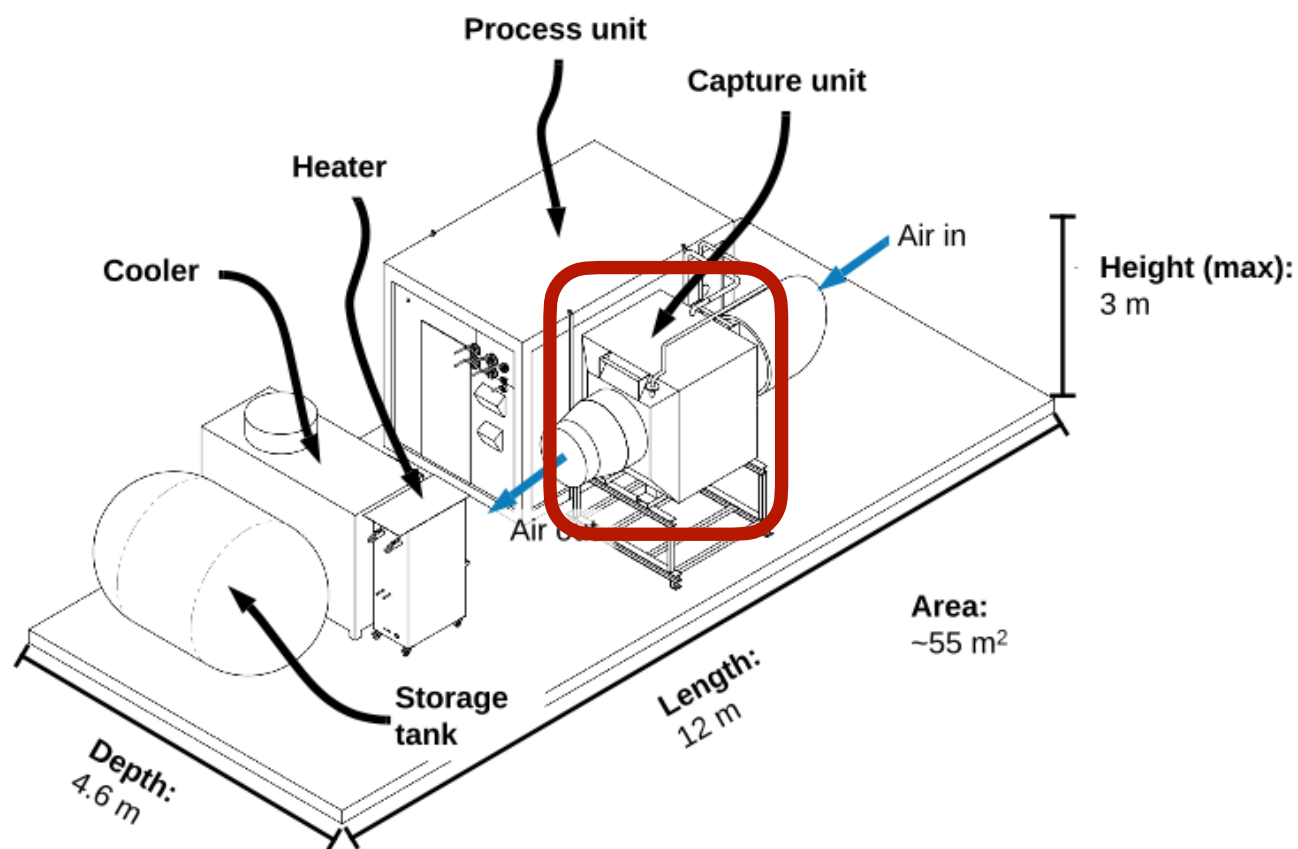
- 1 m³ of air contains ~0.75 grams of CO₂
- To capture T tons of CO₂ per year, a DAC device that captures X % of the CO₂ in the air passing through it, will need to “process” $T / (X * 0.75 \text{ g})$ of air every year.
- If X = 50 % and T = 100 t/y, the value of Y is 8.5 m³/s.
- This size of the facility depends on the air flow velocity through the system.
- At 1 m/s, the minimum theoretical requirement is 8.5 m² of “*intake area*” per 100 t/y, at 4 m/s, just ~2 m².
- Systems spends 60-70 % of the year capturing, meaning figures need to be multiplied by ~1.5.

Approximate size of 100 t/y facility

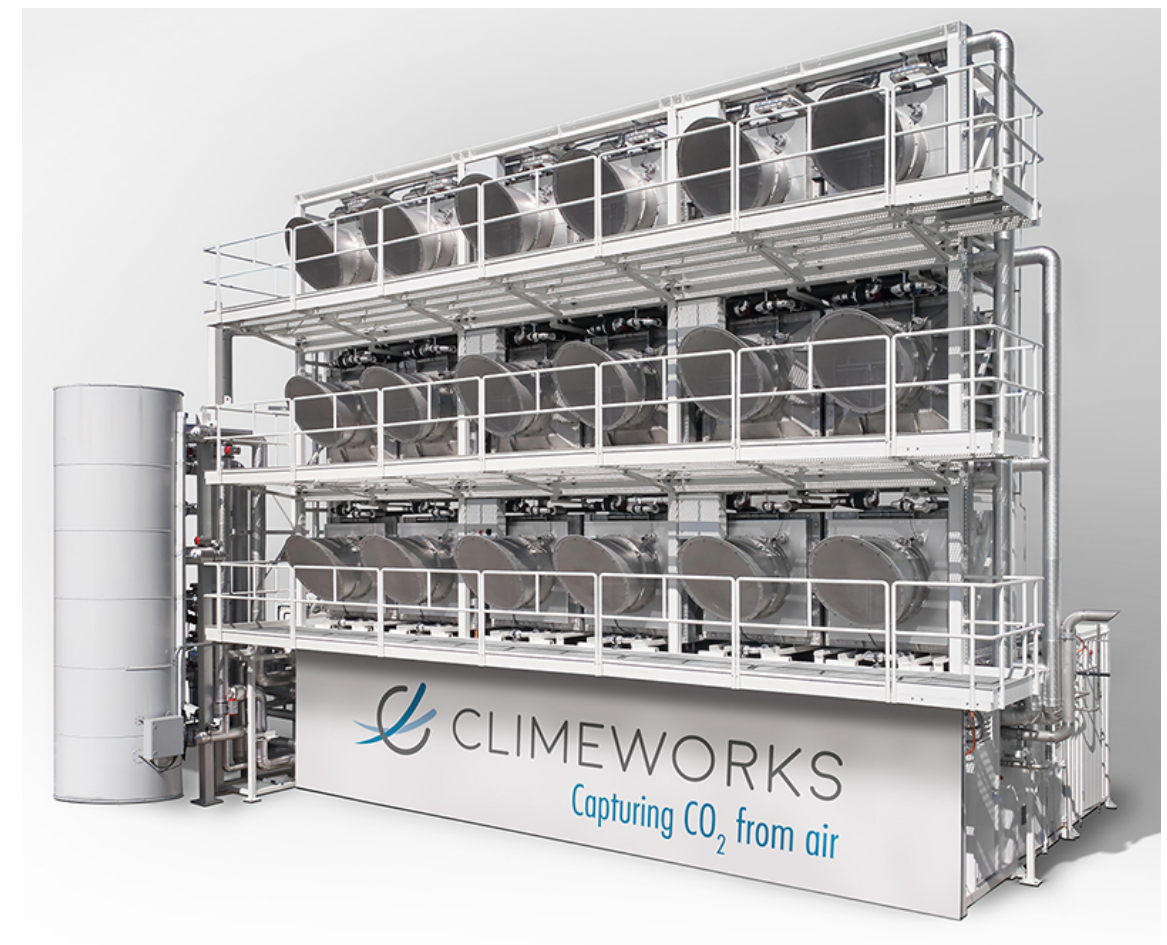


Climeworks size for scale

20 tons/year



500 tons/year



Scaling to 1 MT/y

- Each DAC contactor depletes the air in CO₂, i.e they cannot be placed directly behind one another
- ~250 meter downwind separation ensures good air mixing
- 1 MT/y square-shaped plant with no vertical stacking requires ~1 x 1 km of area
- Vertically stacking 5 units (~10 meters high) requires ~0.1 x 1 km area or ~0.5 x 0.5 km square shaped