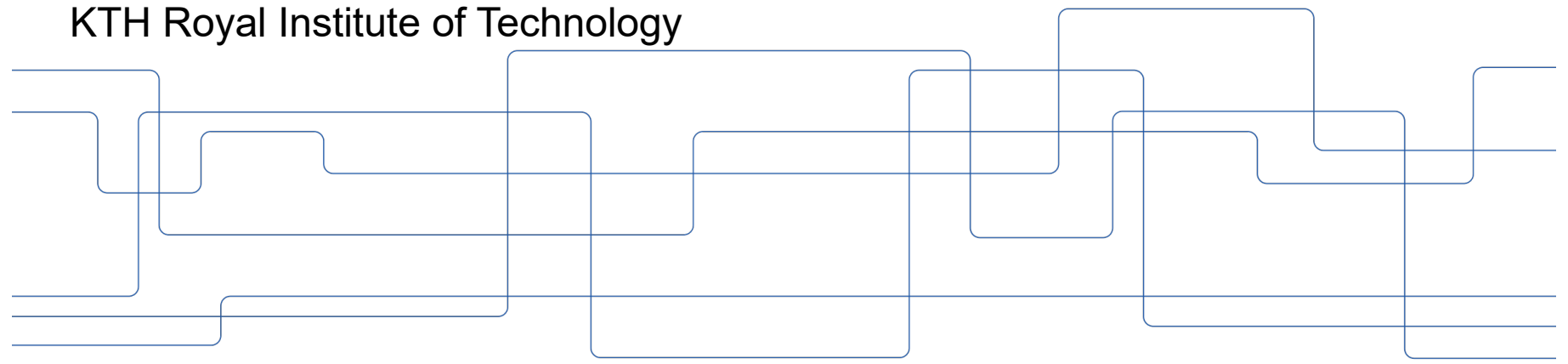




# Heat-Transfer Intensification for Heat-Harvesting, some examples of research done at KTH

Christophe Duwig

Dept. Chemical Engineering, KTH Energy Platform & KTH Climate Action Centre  
KTH Royal Institute of Technology





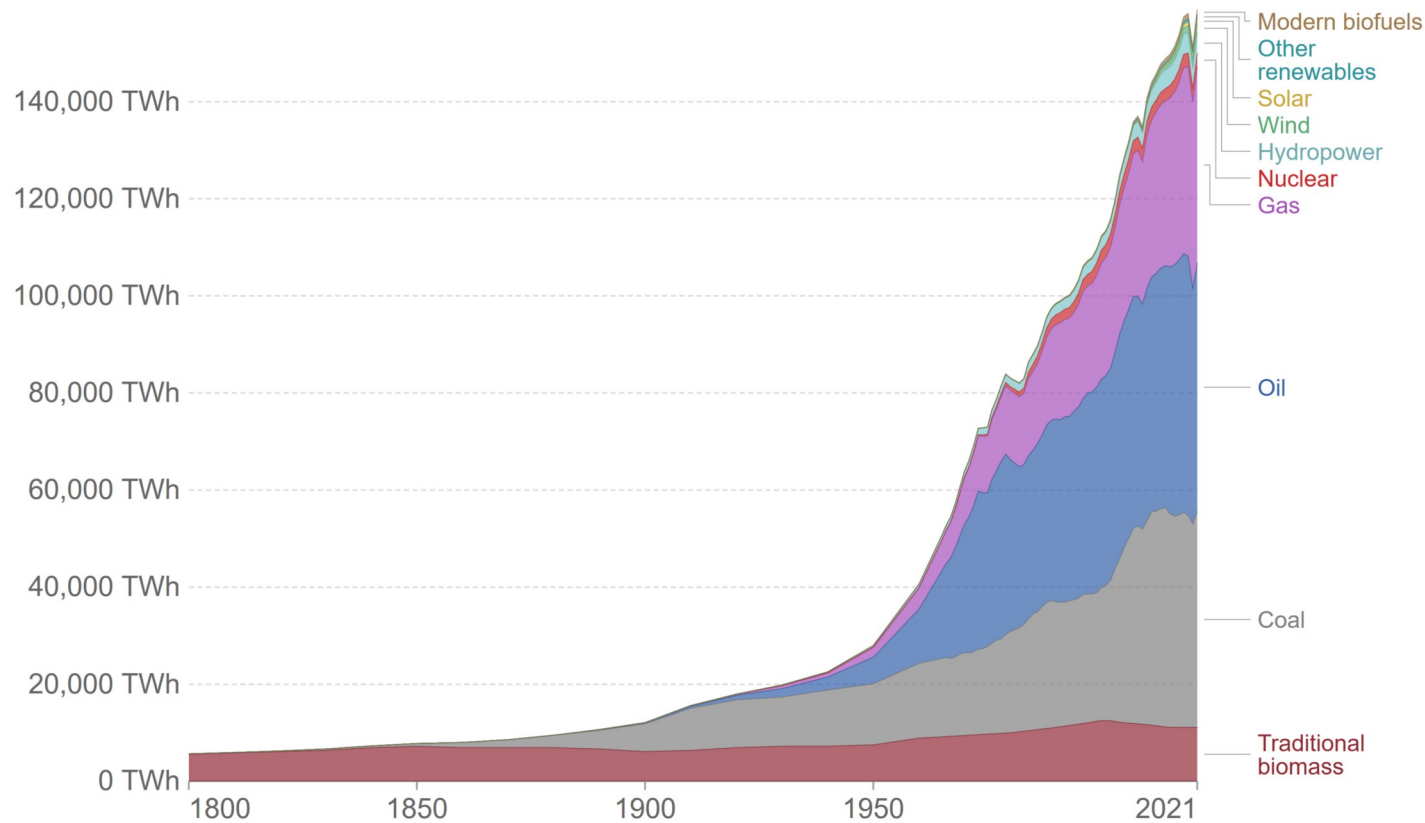
# Short Presentation



- My day jobs
  - Professor at the division of Process Technology, KTH Chemical Engineering
  - Visiting Prof. at the Division of Building Technologies and Design, KTH ABE
  - Vice-Director of the KTH Energy Platform ... mostly covering at "heat"
  - Lead faculty at the KTH Climate Action Centre, topics of Energy & Negative Emissions
- Research
  - High-fidelity simulations of turbulent heat-transfer, phase-change & chemical reactions
  - Data analysis using unsupervised learning alg. (t-sne, UMAP, KMEAN, ...)
  - Heat-Harvesting /Heat-Exchanger technology (additive manufacturing)
  - Negative Emissions, BeCCS, CO<sub>2</sub> Capture
  - Cooling of electric/ electronic systems/ Decarbonization
  - Collaborations: Hitachi Energy, ABB, Stockholm Exergy, TetraPak, AMEXCI, 3Nine, Paebbl, ...

# Global direct primary energy consumption

Direct primary energy consumption does not take account of inefficiencies in fossil fuel production.



Source: Our World in Data based on Vaclav Smil (2017) and BP Statistical Review of World Energy

OurWorldInData.org/energy • CC BY

# Kaya Identity

- Introduced by the Japanese energy economist Yoichi Kaya in 1997 to understand the factors controlling CO<sub>2</sub> emissions

$$CO_2 = \frac{CO_2}{E} \times \frac{E}{GDP} \times \frac{GDP}{P} \times P$$

CO<sub>2</sub> emissions  
by unit energy

energy per income

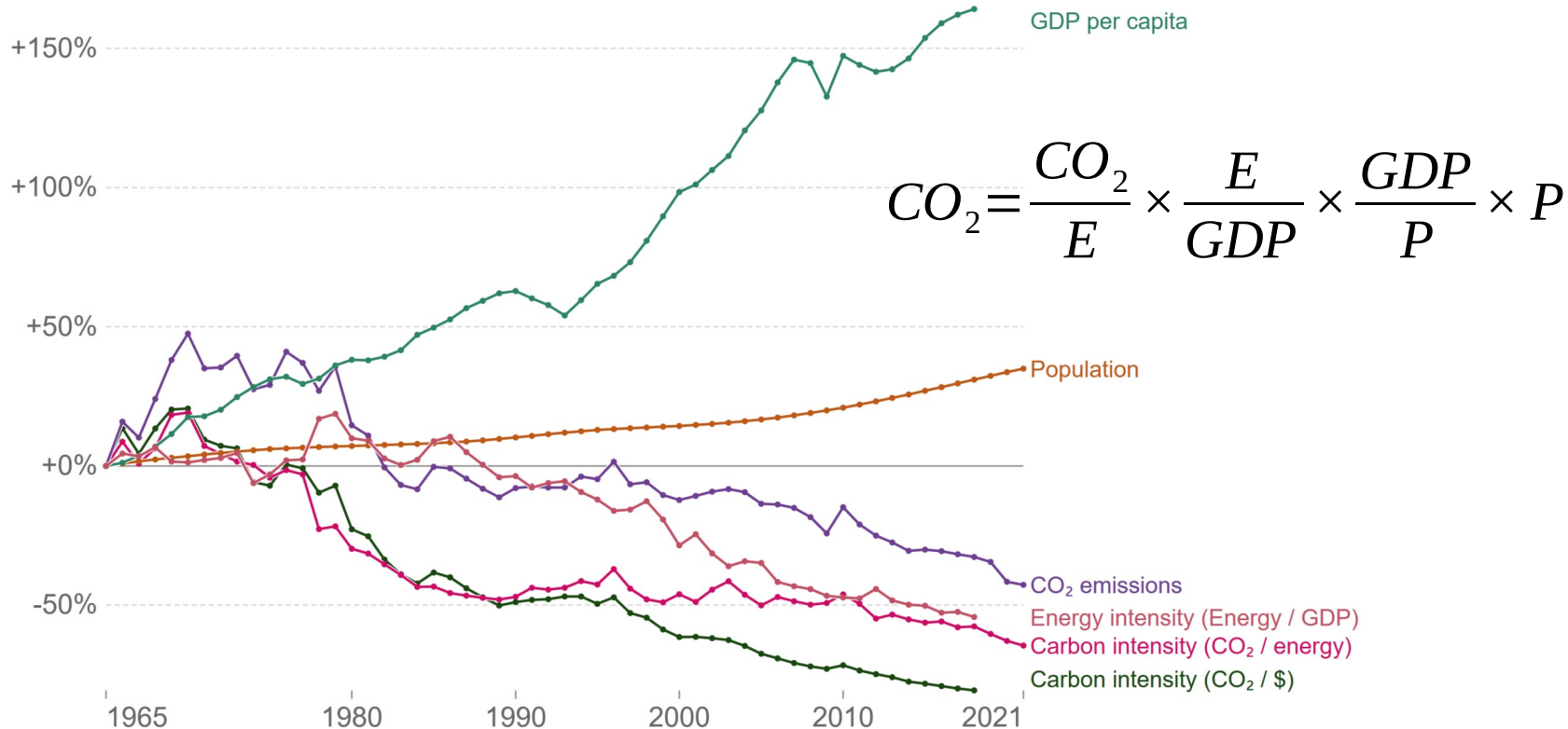
GDP per  
capita

- E is energy used, GDP is a measure of income, P is the population

- Note that  $\frac{1}{4} = \frac{CO_2}{E} \times \frac{1}{2} \times 2.2 \times 1.3 \Rightarrow \frac{CO_2}{E} = \frac{1}{5.7}$

# Kaya identity: drivers of CO<sub>2</sub> emissions, Sweden

Percentage change in the four parameters of the Kaya Identity, which determine total CO<sub>2</sub> emissions. Emissions include fossil fuel and industry emissions<sup>1</sup>. Land use change is not included.



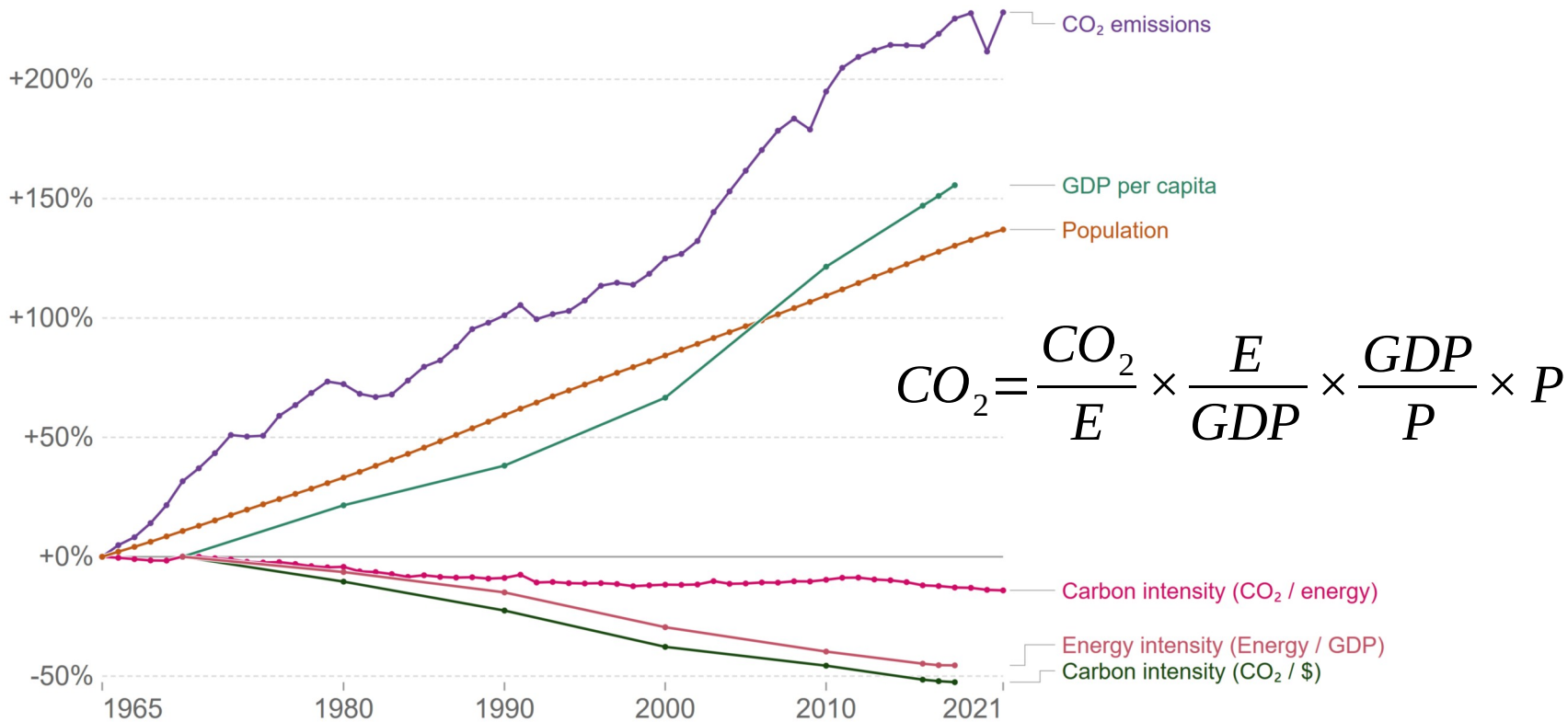
Source: Our World in Data based on Global Carbon Project; UN; BP; World Bank; Maddison Project Database

Note: GDP per capita is measured in 2011 international-\$ (PPP). This adjusts for inflation and cross-country price differences.

OurWorldInData.org/co2-and-other-greenhouse-gas-emissions • CC BY

# Kaya identity: drivers of CO<sub>2</sub> emissions, World

Percentage change in the four parameters of the Kaya Identity, which determine total CO<sub>2</sub> emissions. Emissions include fossil fuel and industry emissions<sup>1</sup>. Land use change is not included.

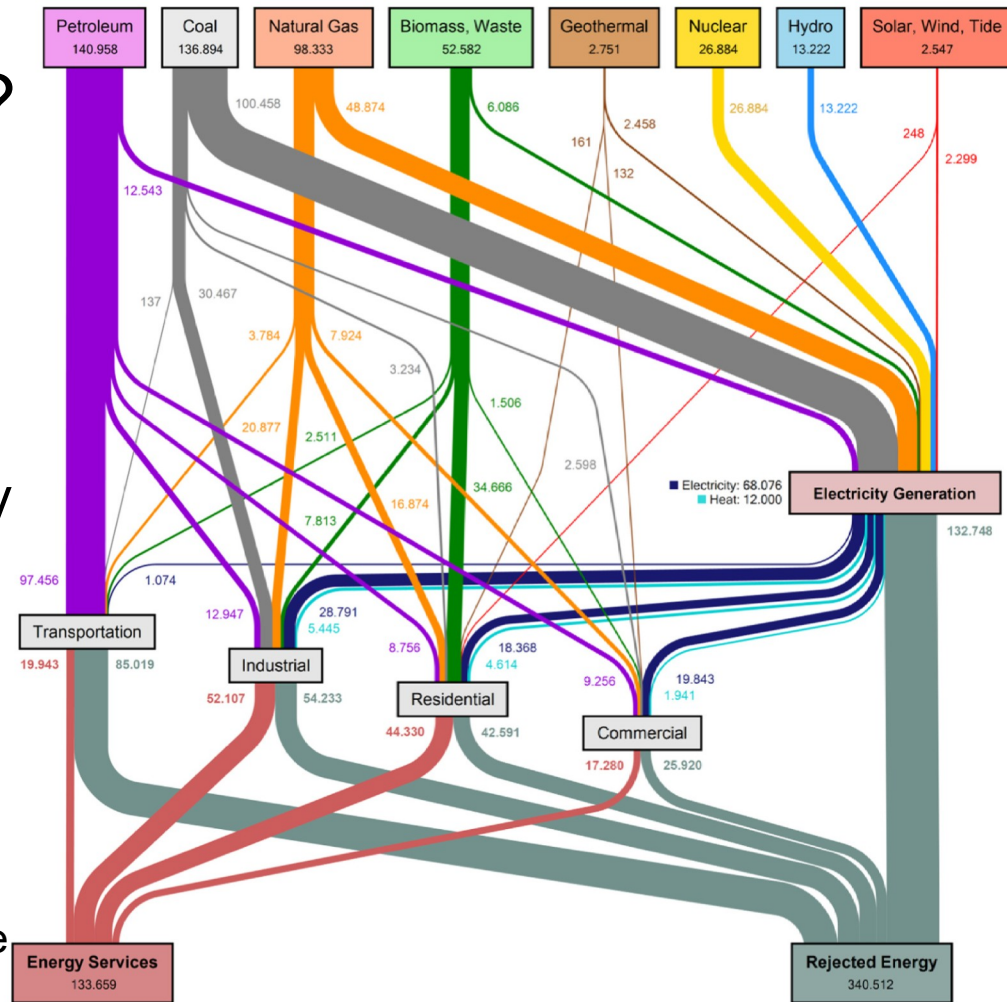


Source: Our World in Data based on Global Carbon Project; UN; BP; World Bank; Maddison Project Database  
 Note: GDP per capita is measured in 2011 international-\$ (PPP). This adjusts for inflation and cross-country price differences.  
 OurWorldInData.org/co2-and-other-greenhouse-gas-emissions • CC BY



# $\frac{E}{GDP}$ ? Service or not?

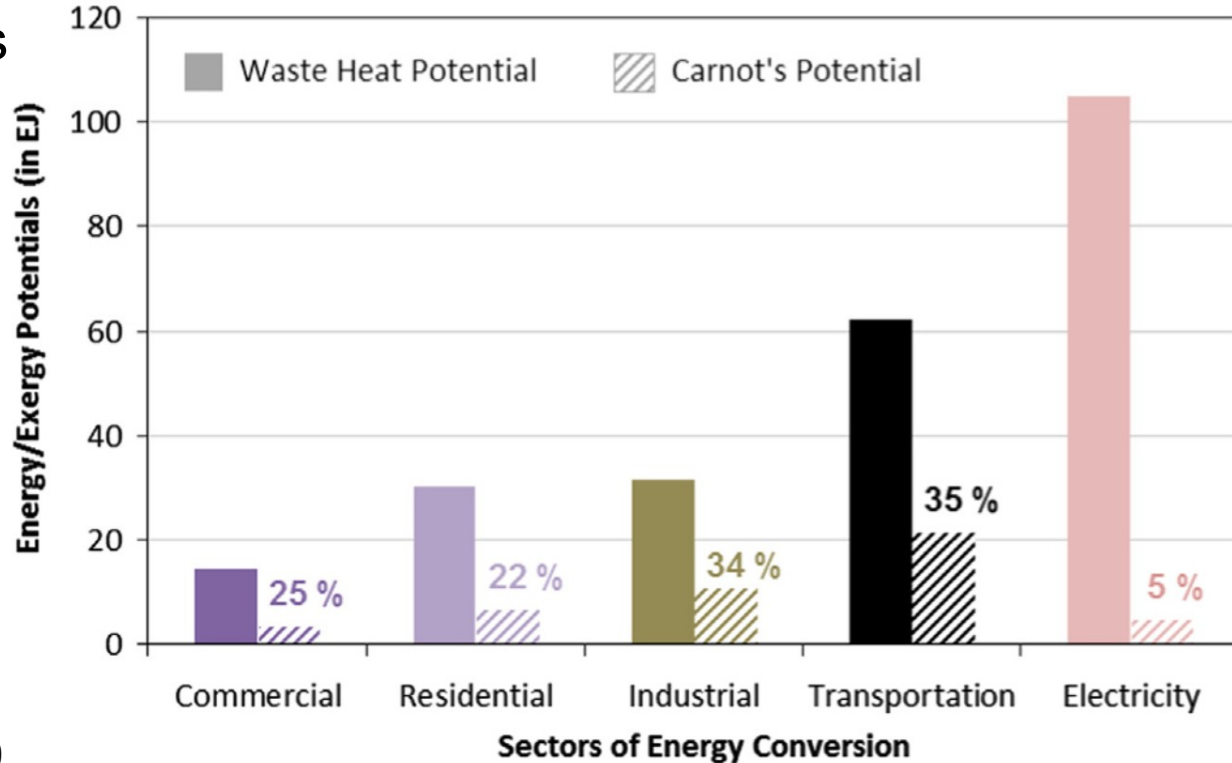
- In 2012, the world used 474 PJ
- ~70% did not offer any service
- Be careful that it is NOT Exergy
- Of course, we need to understand the second principle of thermodynamics





# Energy is not the same than Exergy

- Effluents' temp. matters
- Transportation has the highest potential, industry also!!
- Electrification will help but is not enough
- C. Forman et al. / Renewable and Sustainable Energy Reviews 57 (2016) 1568–1579







# What about electrification?

- Electrified processes or vehicles have lower losses
- Sweden uses about 135 TWh of electricity today
- Electrification will require more electricity, about 200 TWh in 2045
- Complete decarbonization of the mining sector might increase the demand to 240-250 TWh in 2045
- What about residual heat?
  - **40 TWh of electric power to produce H2 by electrolysis gives about 16 TWh of unused heat < 100°C**
  - **2%-6% transmission losses gives 5-15 TWh of cooling/ losses < 100°C**
  - **Still there but at lower temperatures**

[https://www.svensktnaringsliv.se/english/future-electricity-supply-in-sweden\\_1171800.html](https://www.svensktnaringsliv.se/english/future-electricity-supply-in-sweden_1171800.html)



Transformers at substation near Denver International Airport, Colorado – Wikimedia commons

# Learning from Kaya Identity

$$CO_2 = \frac{CO_2}{E} \times \frac{E}{GDP} \times \frac{GDP}{P} \times P$$

Decarbonation  
Electrification  
Hydrogen  
Biofuels  
Nuclear  
Renewables

Efficiency, Use Heat-Pumps, Stop waste, Smart Systems, Energy Storage, Integration,...

Policies, habits, values and democratic decisions

*Over-consumption*  
*Sufficiency*



# Carnot's take on efficiency

- Given a hot source at  $T_H$  and a cold source at  $T_C$
- In general high efficiency is expected for high temperature source, e.g. combustion
- In a perfect world, the maximum efficiency is

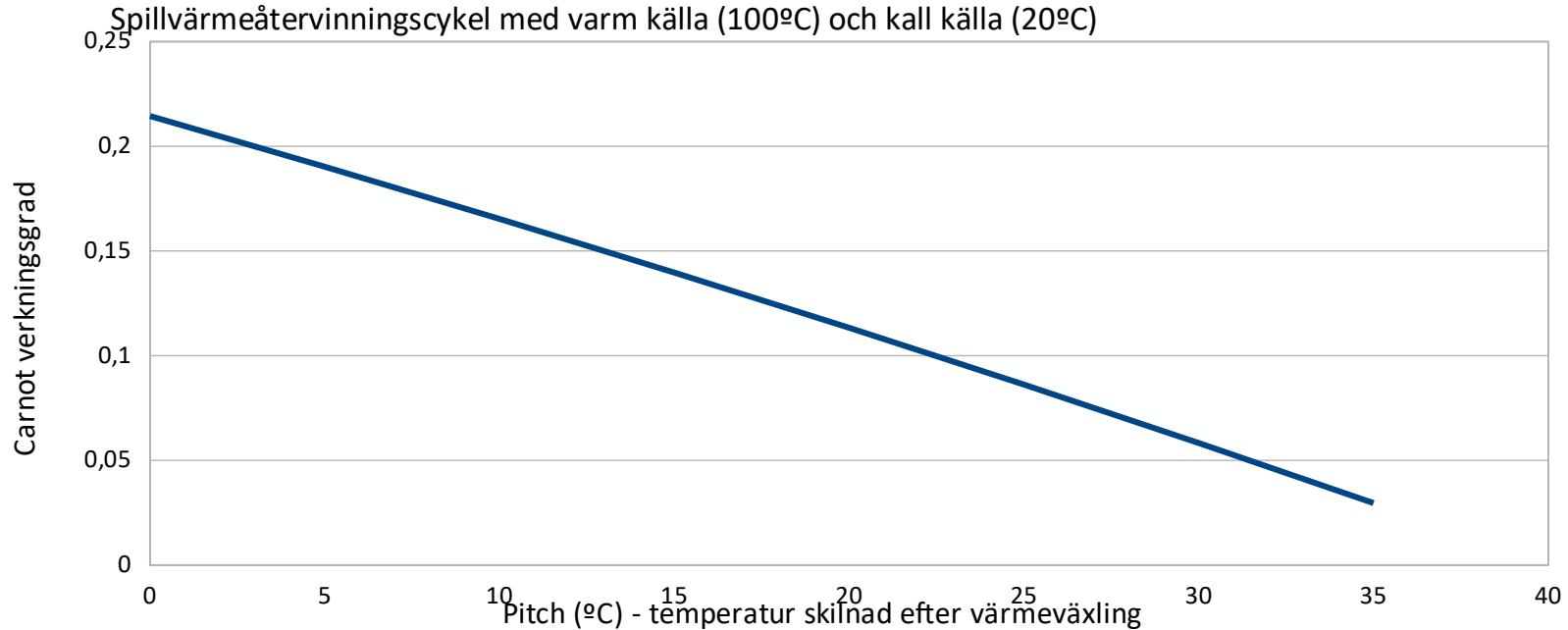
$$\eta = 1 - T_C/T_H$$

---



# In a real(er) world

- $\Delta T$  is a temperature difference across the Heat-Exchanger
- It gives:  $\eta = 1 - (T_C + \Delta T) / (T_H - \Delta T)$





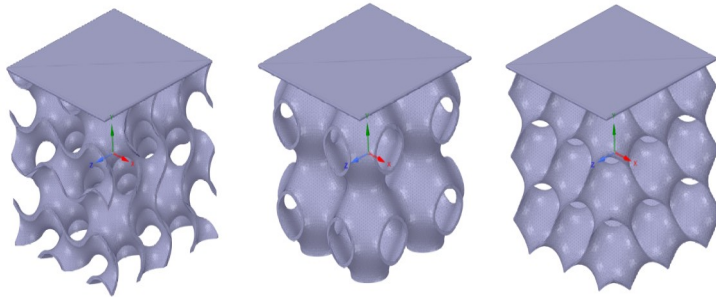
# Heat-Transfer intensification

- $Q = A \cdot h \cdot \Delta T$
  - with  $h = f(\text{Re}, \text{Pr}, \dots)$
  - Increasing heat-transfer can be done by
    - Increasing  $A$  (but not making the device too big)
    - Increasing  $h$  (but there a limits in  $\text{Re}$ )
  - Same  $Q$  with lower  $\Delta T \rightarrow$  increase  $A$  and/or  $h$
-



# Increasing $A$ in a compact manner

- Additive manufacturing opens new avenues for designing energy and material efficient heat-exchangers
- Triple Periodic Minimum Surfaces are one strong candidate family



- The optimal heat transfer performance of the heat exchanger may vary depending on,
    1. TPMS cell architecture,      Periodic length,
    2. Wall thickness,                      Orientation angle,
    3. Offset parameter,                      Set-up configuration,
    4. Fabrication limitations,              Selection of the best TPMS material and thermal properties,
    5. Selection of the best working fluid, hazardness and thermal properties.
-

# Case Study #1 (Effect of TPMS wall thickness)

International Journal of Heat and Mass Transfer 177 (2021) 121415

Contents lists available at ScienceDirect



International Journal of Heat and Mass Transfer

journal homepage: [www.elsevier.com/locate/hmt](http://www.elsevier.com/locate/hmt)



## Design analysis of the “Schwartz D” based heat exchanger: A numerical study

Reza Attarzadeh\*, Marc Rovira, Christophe Duwig

Department of Chemical Engineering, Royal Institute of Technology (KTH), Stockholm, Sweden

### ARTICLE INFO

#### Article history:

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#### Keywords:

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Triply periodic minimal surface

Schwartz D

Conjugate heat transfer

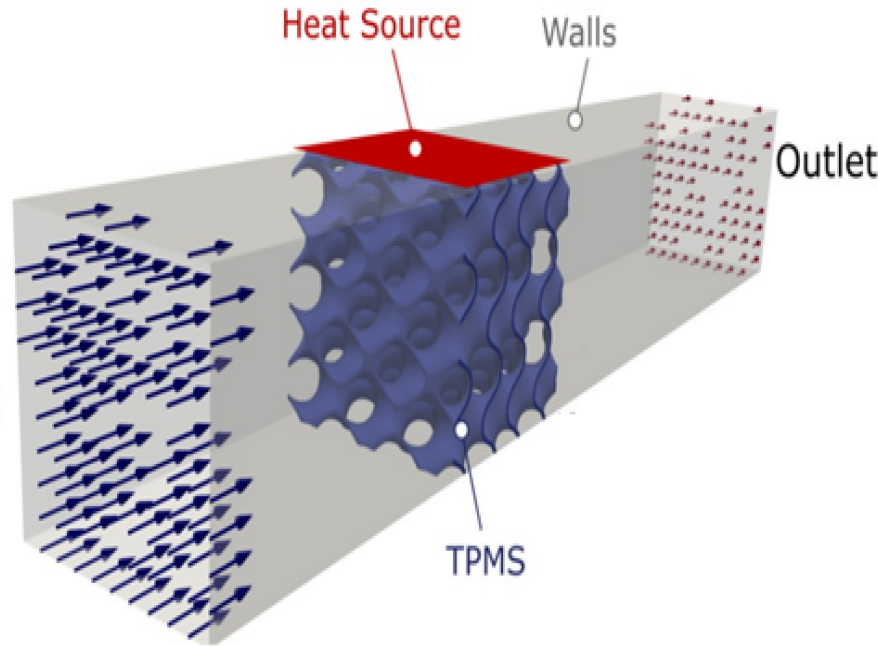
Heat exchanger

### ABSTRACT

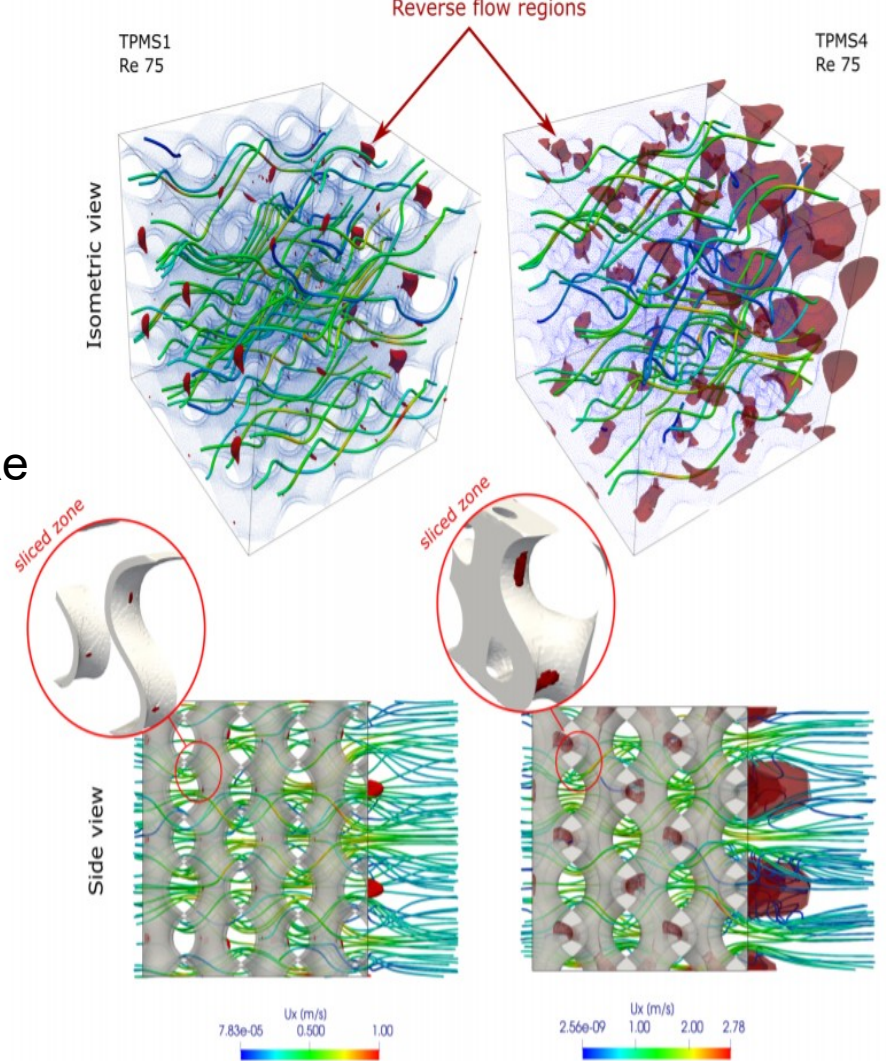
Triply Periodic Minimal Surfaces (TPMS) have promising thermophysical properties, which makes them a suitable candidate in the production of low-temperature waste heat recovery systems. A TPMS thermal performance is connected to the complex flow patterns inside the pores and their interactions with the walls. Unfortunately, the experimental study's design analysis and optimization of TPMS heat exchangers are complicated due to the flow pattern complexity and visual limitations inside the TPMS. In this study, three-dimensional steady-state, conjugate heat transfer (CHT) simulations for laminar incompressible flow were carried out to quantify the performance of a TPMS based heat exchanger. TPMS Lattices based on Schwartz D architecture was modeled to elucidate the design parameters and establishing relationships between gas velocity, heat transfer, and thermal performance of TPMS at different wall thicknesses. In this study, four types of lattices from the same architectures with varying wall thickness were examined for a range of the gas velocity, with one design found to be the optimized lattice providing the highest thermal performance. The results and methodology presented here can facilitate improvements in TPMS-heat exchangers' fabrication for recycling the waste heat in low pitch thermal systems.

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- Low reverse flow regions
- High heat-transfer rate even at low Re
- Many interesting observations
- Quantification of these behaviors







Applied Thermal Engineering 212 (2022) 118448



Contents lists available at [ScienceDirect](#)

## Applied Thermal Engineering

journal homepage: [www.elsevier.com/locate/ate](http://www.elsevier.com/locate/ate)



Research paper

# Multi-objective optimization of TPMS-based heat exchangers for low-temperature waste heat recovery

Reza Attarzadeh <sup>a,\*</sup>, Seyed-Hosein Attarzadeh-Niaki <sup>b</sup>, Christophe Duwig <sup>a</sup>

<sup>a</sup> Department of Chemical Engineering, Royal Institute of Technology (KTH), Stockholm, Sweden

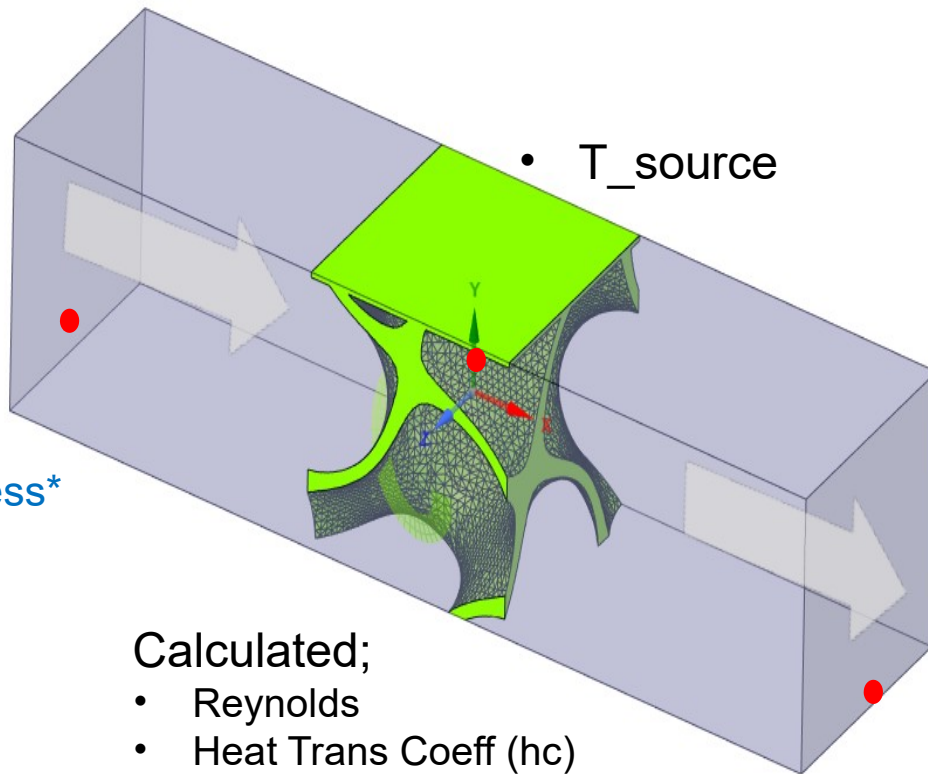
<sup>b</sup> Faculty of Computer Science and Engineering, Shahid Beheshti University (SBU), Tehran, Iran





# DOE & Optimization

- $U_{in}$
- $T_{in}$
- $P_{in}$
- Density
- Viscosity
- TPMS thickness\*
- TPMS length\*



Calculated;

- Reynolds
- Heat Trans Coeff ( $h_c$ )
- Nussult ( $Nu$ )
- $\Delta T = T_{source} - T_{out}$
- $\Delta P = P_{out} - P_{in}$

- $U_{out}$
- $T_{out}$
- $P_{out}$

\* Excluded



# Summary of OP design

## Optimization Study

Maximize	Goal is to Maximize Temperature difference
Minimize	Goal is to Minimize Pressure difference
$\leq 150$	Strict Constraint, Reynolds less than or equals to 150

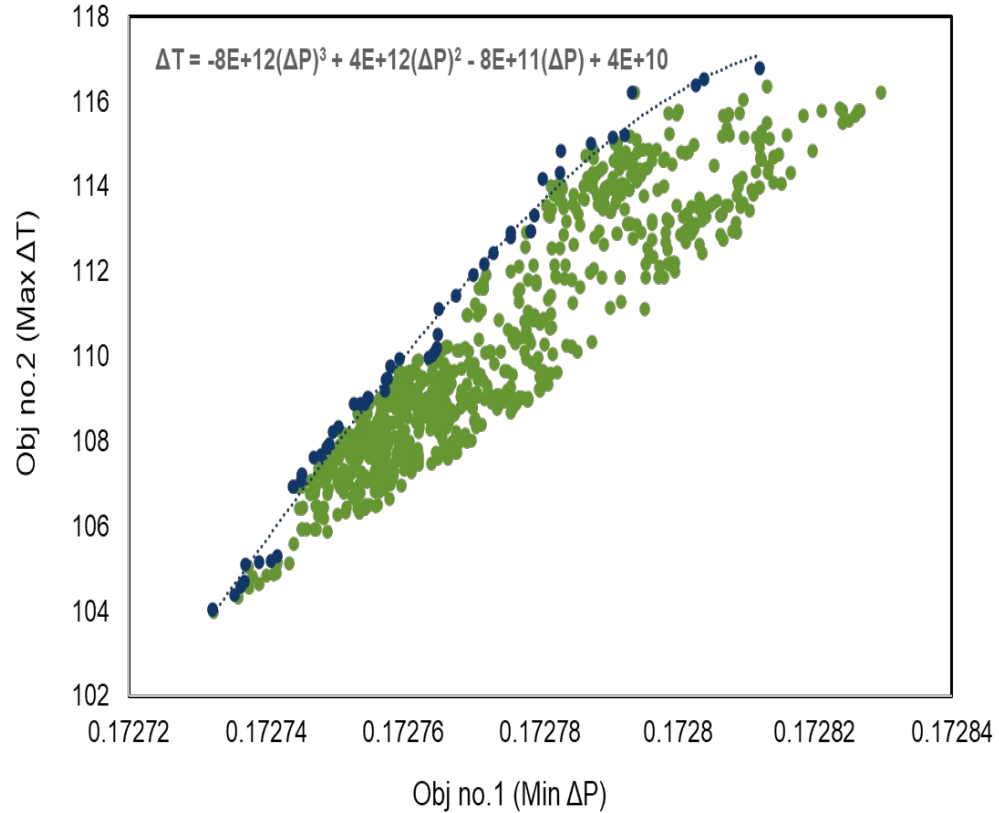
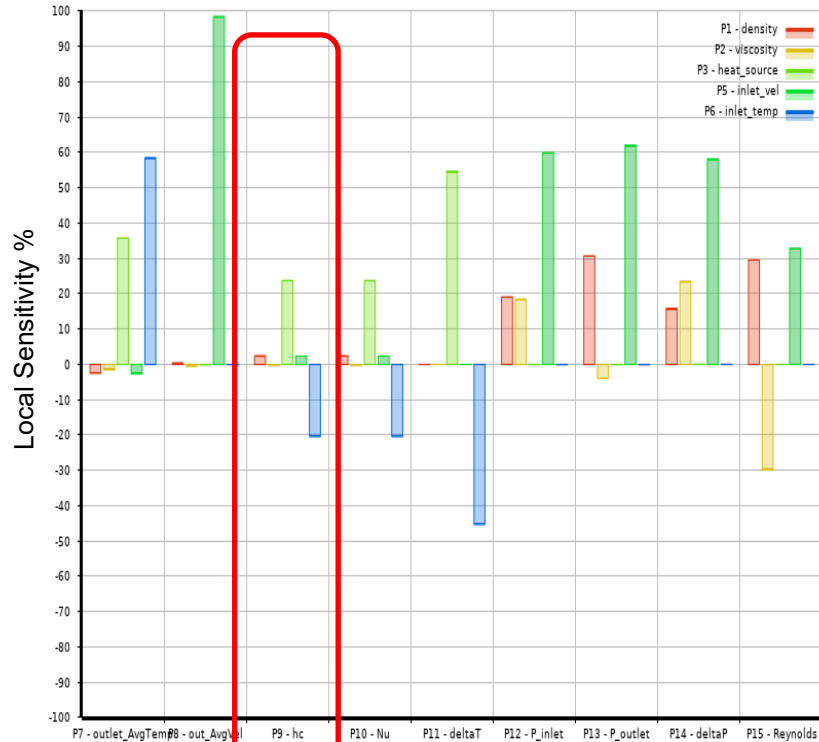
## Optimization Method

MOGA	Multi-Objective Genetic Algorithm
Configuration	Generate 7000 samples initially, 1400 samples per iteration
Status	Converged after 28797 evaluations.

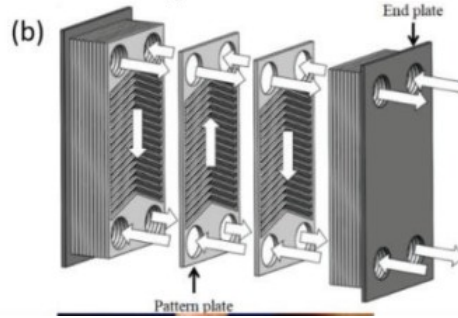
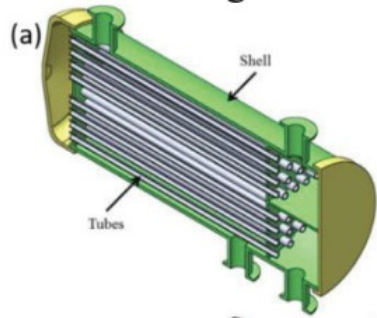


# Sensitivity and Pareto front

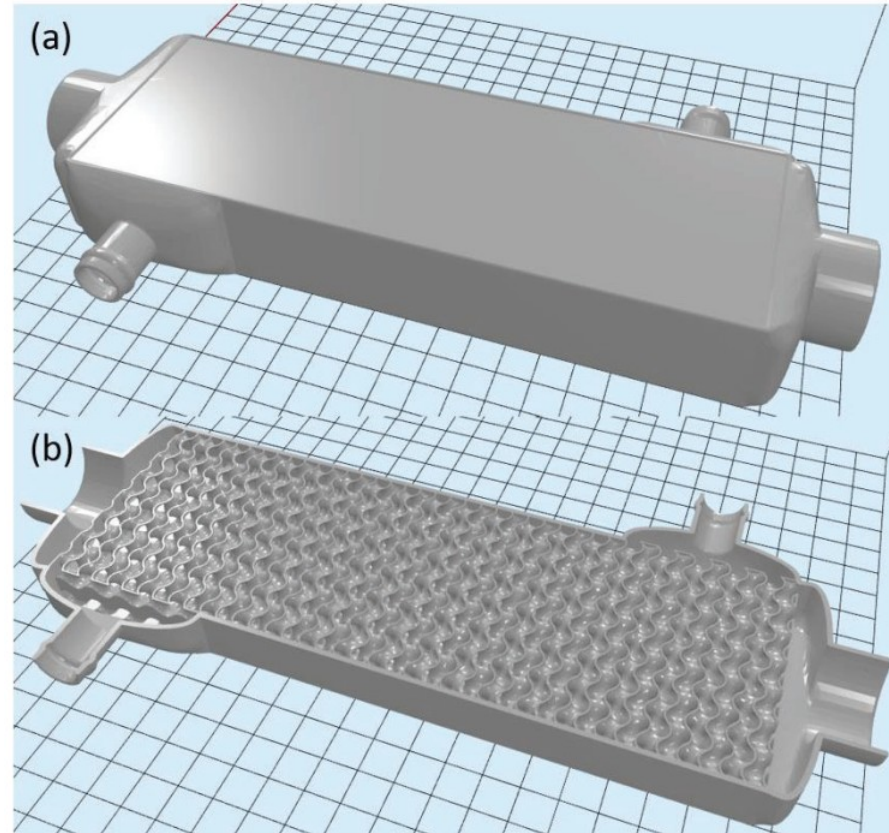
Heat transfer Coefficient (hc)



# Next step 2 fluids TPMS



Present solutions





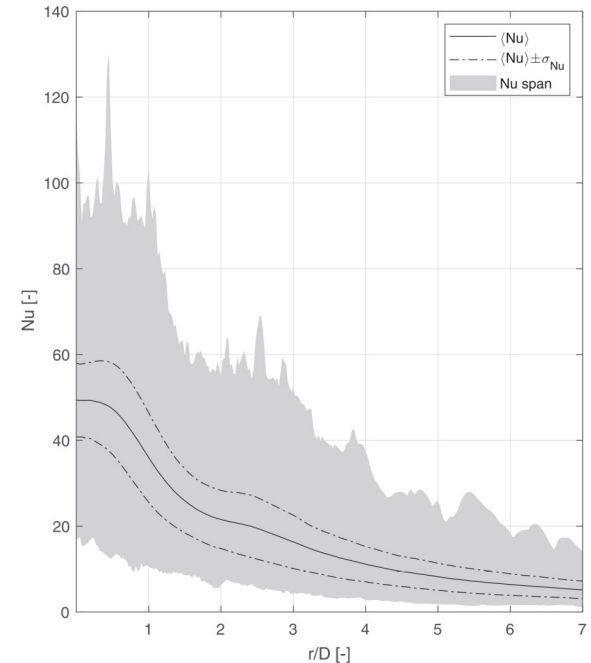
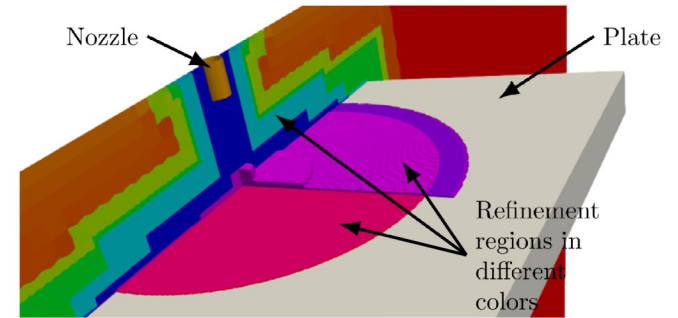
# Increasing $h$ – playing with turbulence

Relaminarization is often a problem

Heat-transfer is driven by turbulence and in particular by large scale structures

We look at the flow with high-fidelity simulations

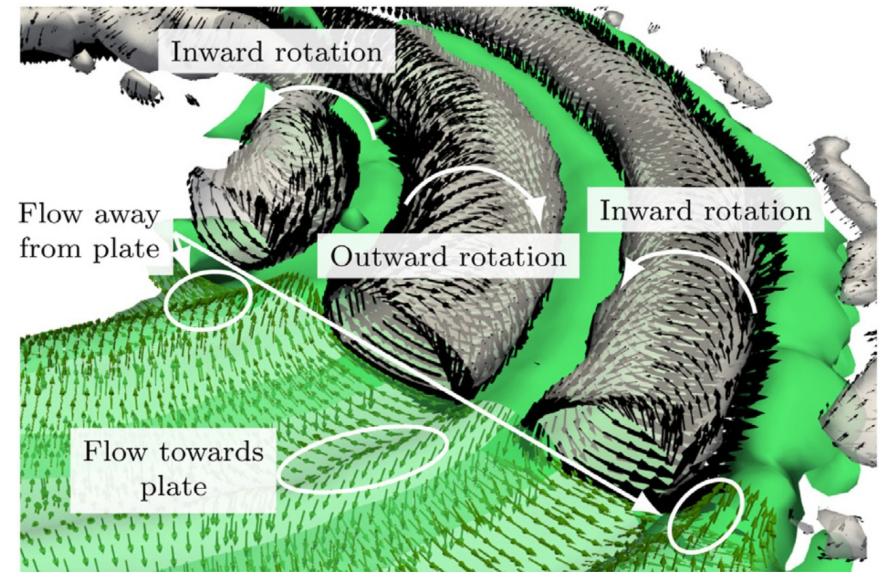
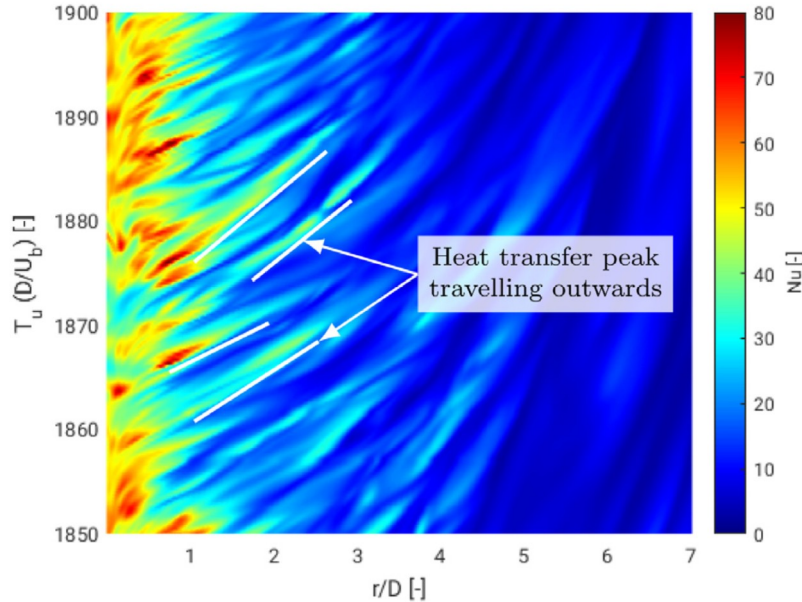
*K. Rönnberg and C. Duwig International Journal of Heat and Mass Transfer 173 (2021) 121197*





# Increasing $h$ – playing with turbulence

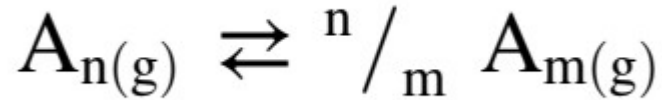
High  $Nu$  is correlated with outward travelling vortices





# Increasing $h$ - Reactive fluids

Reversible equilibrium reactions



Reaction is endothermic – it takes energy to break the large molecule

Reaction is pushed right by higher temperatures and left by higher pressures

It is gas phase all the time

Example

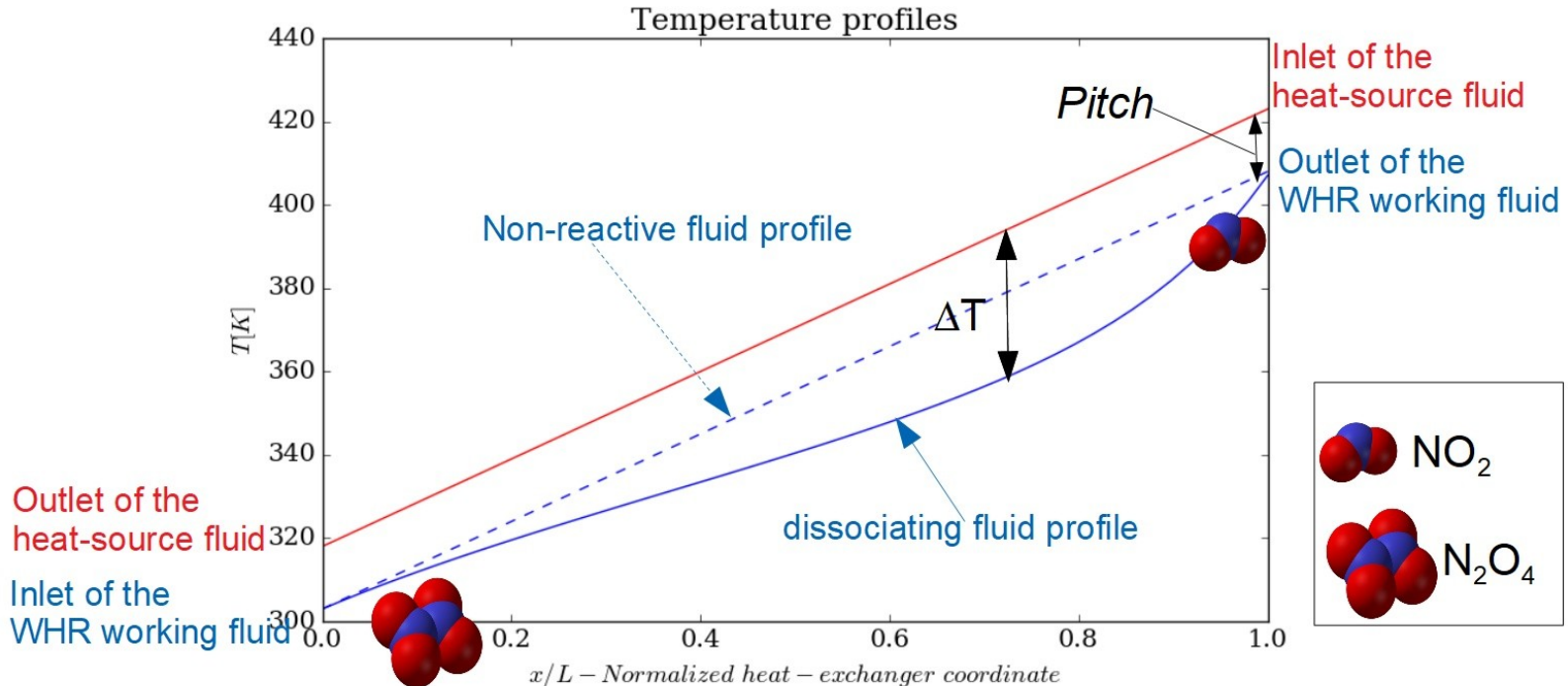
- $N_2O_4 = 2 NO_2 = 2 NO + O_2$
  - $NOCl = NO + \frac{1}{2} Cl_2$
-





# Reactive fluids

## Temperature profiles in an HTX



# Effect of dissociation reactions on heat-transfer

International Journal of Heat and Mass Transfer 182 (2022) 121946



Contents lists available at [ScienceDirect](https://www.sciencedirect.com)

International Journal of Heat and Mass Transfer

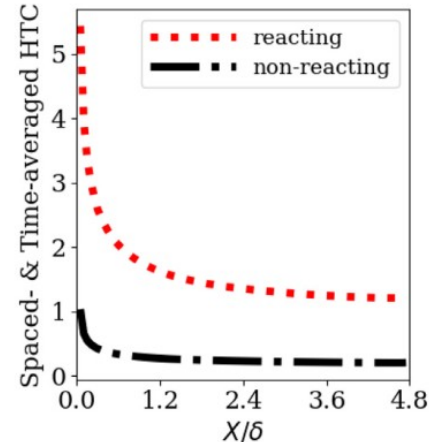
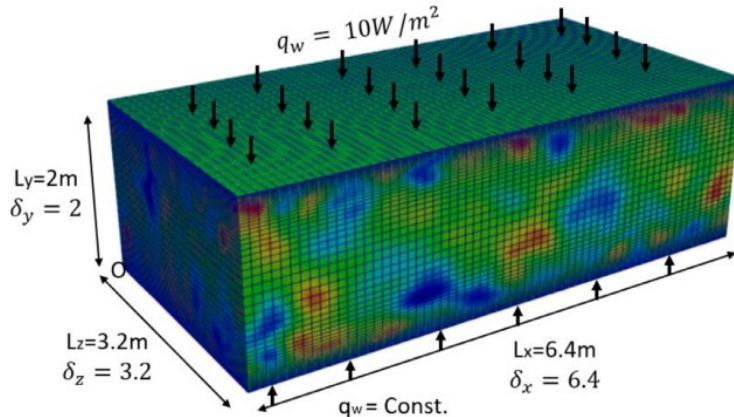
journal homepage: [www.elsevier.com/locate/hmt](http://www.elsevier.com/locate/hmt)



Identification of heat transfer intensification mechanism by reversible  $N_2O_4$  decomposition using direct numerical simulation

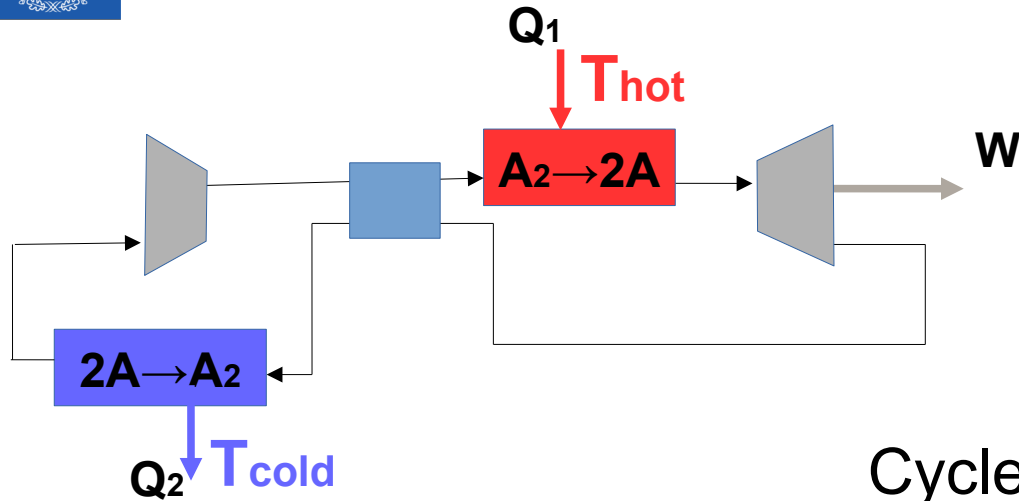
Kai Zhang\*, Yazhou Shen, Christophe Duwig

Department of Chemical Engineering, Royal Institute of Technology (KTH), Brinellvägen 8, 114 28 Stockholm, Sweden



Boosts  
Heat-  
transfer  
by +500%

# Impact on the thermodynamic cycle



Cycle efficiency  $N_2O_4$

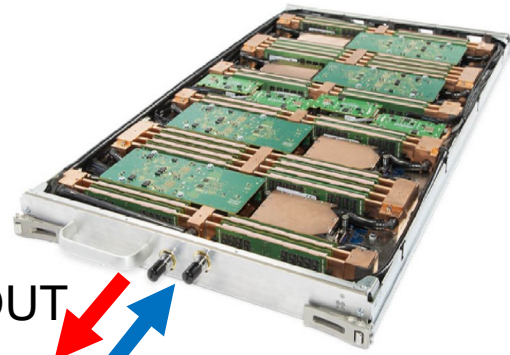
- $\eta = 0.09$  @  $T_{hot} = 363K$
- $\eta = 0.12$  @  $T_{hot} = 393K$

Rapid response to transient

Potentially very compact HTX



# Electronic cooling



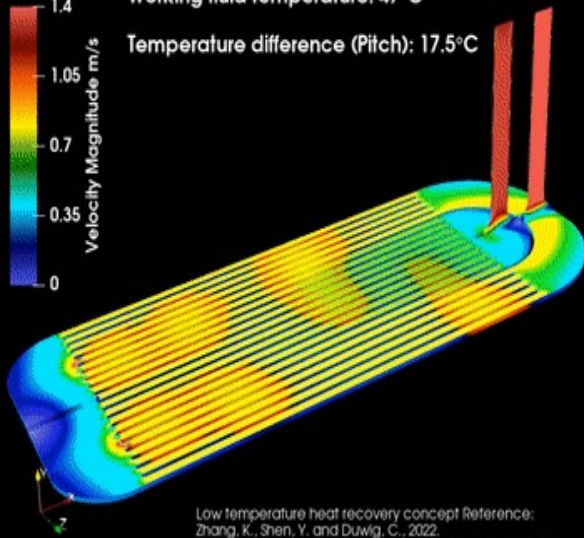
Presenter: Dr. Kai Zhang, KTH, Sweden.  
Co-authors: Lailinen Iupo, Aalto, Finland.  
Prof. Ville Anton Vuorinen, Aalto, Finland.  
Prof. Christophe Duwig, KTH, Sweden.



HTX Wall temperature: 59.5°C

Working fluid temperature: 47°C

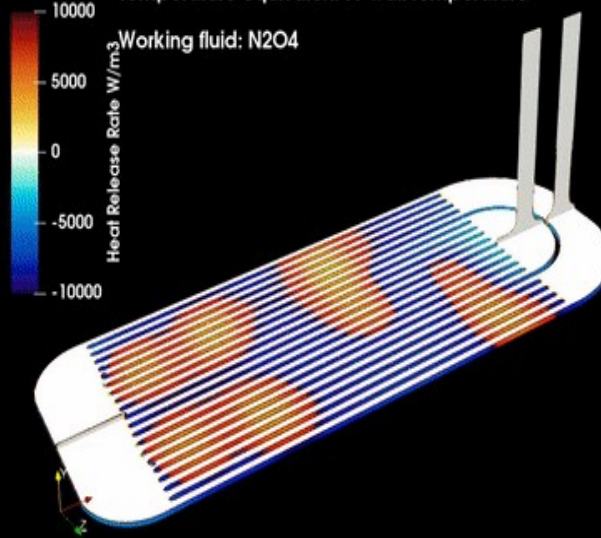
Temperature difference (Pitch): 17.5°C



Big Orange spots: electronic components

Temperature equivalent to wall temperature

Working fluid: N2O4



Low temperature heat recovery concept Reference:  
Zhang, K., Shen, Y. and Duwig, C., 2022.  
Identification of heat transfer intensification mechanism  
by reversible N2O4 decomposition using direct numerical simulation.  
International Journal of Heat and Mass Transfer, 162, p.121946.



# Applications to the built environment

Renewable and Sustainable Energy Reviews 166 (2022) 112625

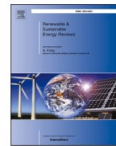


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Contents lists available at [ScienceDirect](#)

Renewable and Sustainable Energy Reviews

journal homepage: [www.elsevier.com/locate/rser](http://www.elsevier.com/locate/rser)



Project in the frame of the IEA Annex 37  
- Smart Design and Control of Energy Storage Systems

Smart design and control of thermal energy storage in low-temperature heating and high-temperature cooling systems: A comprehensive review

Amirmohammad Behzadi<sup>a,\*</sup>, Sture Holmberg<sup>a</sup>, Christophe Duwig<sup>a</sup>, Fariborz Haghighat<sup>b</sup>, Ryozo Ooka<sup>c</sup>, Sasan Sadrizadeh<sup>a,d</sup>

Results in Engineering 16 (2022) 100619



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Contents lists available at [ScienceDirect](#)

Results in Engineering

journal homepage: [www.sciencedirect.com/journal/results-in-engineering](http://www.sciencedirect.com/journal/results-in-engineering)



Project in the frame of the IEA Annex 78  
- Supplementing Ventilation with Gas-phase Air Cleaning, Implementation and Energy Implications

Heating energy implications of utilizing gas-phase air cleaners in buildings' centralized air handling units

Behrouz Nourozi<sup>a,\*</sup>, Sture Holmberg<sup>a</sup>, Christophe Duwig<sup>a</sup>, Alireza Afshari<sup>b</sup>, Pawel Wargocki<sup>c</sup>, Bjarne Olesen<sup>c</sup>, Sasan Sadrizadeh<sup>a,d,\*\*</sup>



*Re-using cleaned indoor air to reduce losses*



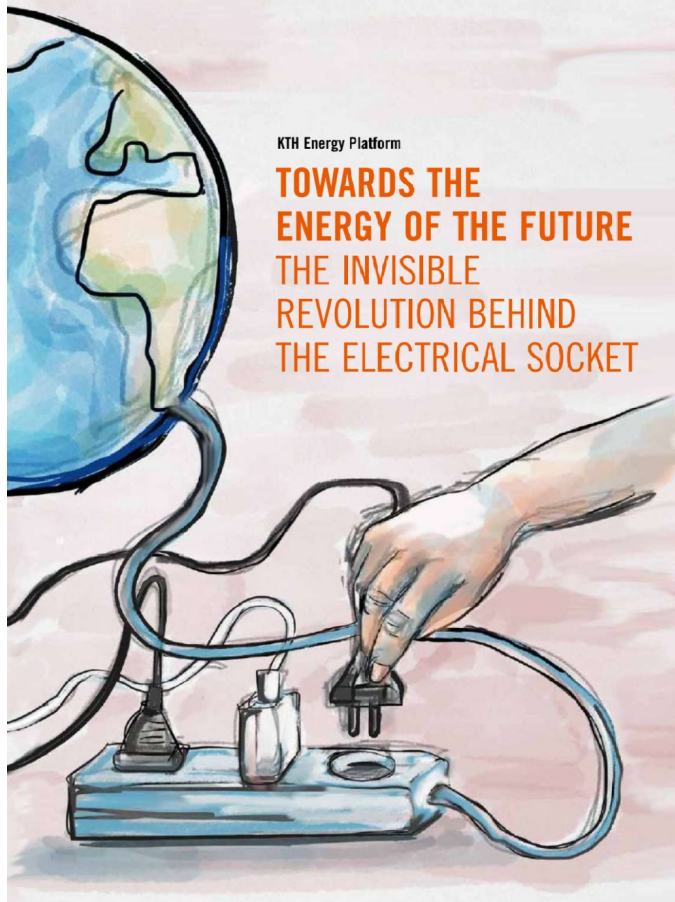
# Energiforsk Värmeklustret

- Happy to hear your areas of interest
- Calls of interests
  - Swedish Energy Agency Termo
  - Swedish Energy Agency E2B2 (energy efficient buildings)
  - Vinnova (Eurostars, ....)
  - .....
- Track for collaboration
  - Heat-Exchanger technology (additive manufacturing)
  - Heat-Harvesting from electric/ electronic systems/ low temp. sources
  - Decarbonize processes
  - PCM – heat storage (flexible buildings)



Contact:  
[duwig@kth.se](mailto:duwig@kth.se)





KTH Energy Platform

## TOWARDS THE ENERGY OF THE FUTURE THE INVISIBLE REVOLUTION BEHIND THE ELECTRICAL SOCKET

Energi finns överallt. Vi tar för givet att den finns tillhands när vi vill värma upp våra hem, laga mat, använda våra datorer, mobiltelefoner, rulltrappor, lyftkranar, röntgenapparater, bussar, tåg, flygplan och bilar. Den är en självklar, ofta osynlig – och tyvärr ohållbar del av våra liv.

Idag vet vi att världens energisystem måste omvandlas i grunden. Det är en förutsättning för att vi ska kunna bromsa klimatförändringarna och skapa ett hållbart samhälle. Och vi har alla viktiga roller att spela i omvandlingen. Men hur förändrar vi något som vi inte kan se?

I den här antologin delar några av Sveriges ledande energiforskare sin syn på kända och mindre kända utmaningar och lösningar kring framtidens energi. Syftet är att stimulera samtal och konstruktiv debatt för att vi ska kunna ta oss an utmaningarna i en öppen dialog där fakta och kunskap formar vår framtid.

Boken är skriven av forskare anslutna till **KTH:s Energiplattform**, i samarbete med den ideella organisationen **Vetenskap & Allmänhet, VA**.



[www.energiantologi.se](http://www.energiantologi.se)



# Thank you and see you next time at the KTH Climate Action House



KTH Climate Action Centre is a multi-disciplinary, collaborative and research-focused centre aiming to advance climate mitigation and adaptation in synergy with all the UN Sustainable Development Goals.

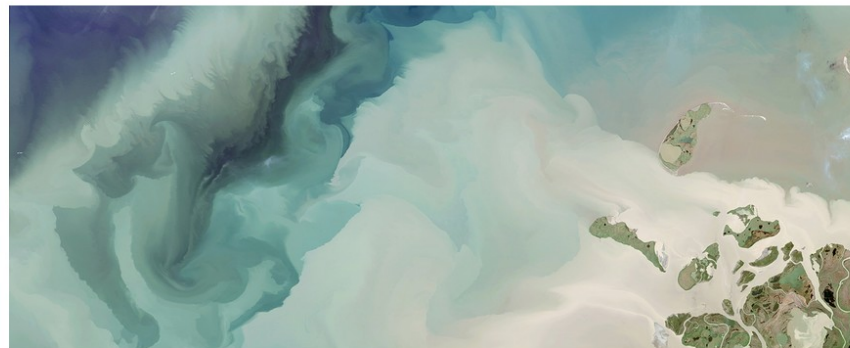


Photo: USGS, Unsplash.

## Vision

The vision of KTH Climate Action Centre is to shape a world with net zero carbon emission and climate resilient and sustainable societies.